

1 **Evaluated kinetic and photochemical data for atmospheric chemistry:**  
2 **Volume IX – gas-phase reactions of halogenated alkanes, alkenes, and**  
3 **oxygenated compounds**

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23 **Abstract.** This article, the ninth in the series, presents kinetic and photochemical data sheets  
24 evaluated by the IUPAC Task Group on Atmospheric Chemical Kinetic Data Evaluation. It  
25 covers an extension of the gas phase and photochemical reactions of halogenated alkanes,  
26 alkenes, and oxygenated organic compounds implemented on the IUPAC website since 2008.  
27 The article consists of a summary table of the recommended kinetic parameters for the  
28 evaluated reactions, and a supplement containing the data sheets providing information upon  
29 which the recommendations are made.

30

31 **1 Introduction**

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33 In the mid-1970s it was appreciated that there was a need to establish an international panel to  
34 produce a set of critically evaluated rate parameters for reactions of interest for atmospheric  
35 chemistry. To this end the CODATA Task Group on Chemical Kinetics, under the auspices of  
36 the International Council of Scientific Unions (ICSU), was constituted in 1977, and tasked to  
37 produce an evaluation of relevant, available kinetic and photochemical data. The first  
38 evaluation by this international committee was published in *J. Phys. Chem. Ref. Data* in 1980  
39 (Baulch et al., 1980) and was followed by supplements in 1982 (Baulch et al., 1982) and 1984  
40 (Baulch et al., 1984). In 1986 the IUPAC Subcommittee on Gas Kinetic Data Evaluation for

41 Atmospheric Chemistry superseded the original CODATA Task Group for Atmospheric  
42 Chemistry. The Subcommittee continued its data evaluation program with supplements  
43 published in 1989 (Atkinson et al., 1989), 1992 (Atkinson et al., 1992), 1997 (Atkinson et al.,  
44 1997a; Atkinson et al., 1997b), 1999 (Atkinson et al., 1999), and 2000 (Atkinson et al., 2000).

45  
46 Starting in 2005, the gas phase evaluation work was expanded to include heterogeneous  
47 reactions of gases on solid (Crowley et al., 2010) and liquid substrates (Ammann et al., 2013).  
48 Aqueous-phase reactions of atmospheric importance were added starting in 2015. The  
49 IUPAC group's work now includes over 1400 gas-phase, heterogeneous, and aqueous-phase  
50 reactions of importance in atmospheric chemistry. Reflecting the broader scope, the group  
51 changed its name to the IUPAC Task Group on Atmospheric Chemical Kinetic Data  
52 Evaluation in 2013. The history of IUPAC data evaluations and their role in addressing the  
53 critical societal challenges of stratospheric ozone loss, tropospheric ozone formation, acid  
54 rain, urban air pollution, aerosol formation, and climate change is discussed by Cox et al.  
55 (2018).

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57 In 2000 the evaluation was made available on the worldwide web (<https://iupac.aeris-data.fr/>).  
58 The IUPAC website hosts an interactive data base with a search facility and hyperlinks  
59 between the summary table and data sheets which can be downloaded as individual PDF files.  
60 Work is underway to provide machine readable metadata from the data sheets to enable  
61 automatic transfer of IUPAC recommended data into atmospheric models. The IUPAC group  
62 continues to update and extend the set of evaluated reactions. To enhance the accessibility of  
63 this updated material to the scientific community, the evaluation is being published as a series  
64 of articles in Atmospheric Chemistry and Physics (Atkinson et al., 2004, 2006, 2007, 2008;  
65 Crowley et al., 2010; Ammann et al., 2013; Cox et al. 2020; Mellouki et al., 2021).

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67 The fourth article in this series covering small ( $\leq C_3$ ) organic halogen species was published  
68 in 2008 (Atkinson et al., 2008). The past two decades have seen increasing concern regarding  
69 the presence of long-chain persistent bioaccumulative fluorinated organic pollutants such as  
70 perfluorooctanoic acid ( $C_7F_{15}C(O)OH$ , PFOA), perfluorooctane sulphonic acid  
71 ( $C_8F_{17}S(O)OH$ , PFOS), and per- and polyfluoroalkyl substances (PFAS) in the environment  
72 (Giesy and Kannan, 2001; Ellis et al., 2004; Lau et al., 2007; Prevedouros et al., 2006).  
73 Concern over the growing contribution of hydrofluorocarbons (HFCs) to radiative forcing of  
74 climate change (Velders et al., 2009) led to the recent Kigali Agreement to limit HFC

75 emissions. Halogenated alkenes and oxygenates have been developed to replace HFCs  
76 (Brown, 2009; Burkholder et al. 2015; Wallington et al., 2015) and are used as industrial  
77 solvents, synthesis reagents for surface coatings, inhalation agents, fire retardants, fire-  
78 fighting foams, and surfactants (Wallington et al., 2017). To provide data relevant to  
79 understanding these new issues we have extended the set of evaluated reactions. We present  
80 here in Volume IX data sheets for gas-phase and photochemical reactions of halogenated  
81 organic species added since publication of Volume IV (Atkinson et al., 2008).

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## 83 **2 Guide to the datasheets**

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85 For each reaction covered in this volume, a datasheet with details about e.g. experimental  
86 methods and a justification of the choice of preferred value is available in the supplementary  
87 information. The datasheets covering gas-phase reactions are principally of two types: (i) those  
88 for individual thermal reactions and (ii) those for the individual photochemical reactions. Rate  
89 coefficients are also known as rate constants, both terms are used here.

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### 91 **2.1 Thermal reactions**

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93 The datasheets begin with a statement of the reactions including all pathways which are  
94 considered feasible. The available kinetic data on the reactions are summarized under two  
95 headings: (i) Absolute Rate Coefficients, and (ii) Relative Rate Coefficients. Under these  
96 headings, we list the published experimental data as absolute rate coefficients. If the  
97 temperature dependence of the rate coefficient has been measured, the results are given in the  
98 temperature dependent form as stated by the authors over a stated temperature range. For  
99 bimolecular reactions, the temperature dependence is usually expressed in the conventional  
100 Arrhenius form,  $k = A \exp(-B/T)$ , where  $B = E/R$ . For a few bimolecular reactions, we have  
101 listed temperature dependences in alternative forms such as  $k = C(T/298 \text{ K})^n \exp(-D/T)$  or  $k =$   
102  $ET^2 \exp(-F/T) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  where the original authors have found that alternative  
103 expressions give a better fit to the data. In our recommendations we seek to provide simple  
104 Arrhenius expressions that describe the kinetics over the atmospherically relevant temperature  
105 range (180-310 K). More complex expressions, which are often needed to describe the  
106 kinetic behaviour over larger ranges of temperature, are given in the Comments on Preferred  
107 Values section in the data sheets. Rate coefficients are given here in units of  $\text{cm}^3 \text{ molecule}^{-1}$   
108  $\text{s}^{-1}$ . Note that “molecule” is not a unit, but is included for clarity. For pressure dependent

109 combination and dissociation reactions, the non-Arrhenius temperature dependence is used.  
110 This is discussed more fully in section 2.3 of this guide. Single-temperature data are presented  
111 as such and, wherever possible, the rate coefficient at, or close to, 298 K as measured by the  
112 original authors is quoted directly. This means that the listed rate coefficient at 298 K may  
113 differ slightly from that calculated from the Arrhenius parameters determined by the same  
114 authors. Rate coefficients at 298 K marked with an asterisk indicate that the value was  
115 calculated by extrapolation of a measured temperature range, which did not include 298 K.  
116 The tables of data are supplemented by a series of comments summarizing the experimental  
117 details. The following abbreviations, relating to experimental techniques, are used in the  
118 Techniques and Comments sections:

- 119 A– absorption
- 120 AS – absorption spectroscopy
- 121 CCD – charge coupled detector
- 122 CIMS – chemical ionization mass spectroscopy/spectrometry
- 123 CL – chemiluminescence
- 124 CRDS – cavity ring-down spectroscopy
- 125 DF – discharge flow
- 126 EPR – electron paramagnetic resonance
- 127 F – flow system
- 128 FP – flash photolysis
- 129 FTIR – Fourier transform infrared
- 130 FTS – Fourier transform spectroscopy
- 131 GC – gas chromatography/gas chromatographic
- 132 HPLC – high-performance liquid chromatography
- 133 IR – infrared
- 134 LIF – laser induced fluorescence
- 135 LMR – laser magnetic resonance
- 136 LP – laser photolysis
- 137 MM – molecular modulation
- 138 MS – mass spectrometry/mass spectrometric
- 139 P – steady state photolysis

140 PLP – pulsed laser photolysis  
141 PR – pulse radiolysis  
142 RA – resonance absorption  
143 RF – resonance fluorescence  
144 RR – relative rate  
145 S – static system  
146 TDLS – tunable diode laser spectroscopy  
147 UV – ultraviolet  
148 UVA – ultraviolet absorption  
149 VUVA – vacuum ultraviolet absorption

150

151 For measurements of relative rate coefficients, wherever possible the comments contain the  
152 actual measured ratio of rate coefficients together with the rate coefficient of the reference  
153 reaction used to calculate the absolute rate coefficient listed in the data table. The absolute  
154 value of the rate coefficient given in the table may be different from that reported by the  
155 original author owing to a different choice of rate coefficient of the reference reaction.  
156 Whenever possible the reference rate data are those preferred in the most recent IUPAC  
157 evaluation of that reaction.

158

159 The preferred values in the datasheets are based on our consideration of the suitability of  
160 experimental method and coverage of applicable parameter space (temperature, total pressure  
161 of diluent gas, partial pressure of gas-phase species) within the atmospherically relevant  
162 range. The general approach and methods used have been reviewed by Cox (2012). It is  
163 recognized that preferred values may change with publication of new data, and such changes  
164 are updated at the website. The preferred rate coefficients are presented (i) at a temperature of  
165 298 K and (ii) in temperature dependent form over a stated temperature range. This is  
166 followed by a statement of the uncertainty limits in  $\log k$  at 298 K and the uncertainty limits  
167 either in  $(E/R)$  or in  $n$ , (for systems with power law temperature dependence), for the mean  
168 temperature in the range. Some comments on the assignment of uncertainties are given later in  
169 this guide to the datasheets. The ‘Comments on Preferred Values’ section describes how the  
170 selection was made and give any other relevant information. The extent of the comments

171 depends upon the present state of our knowledge of the reaction in question. The datasheets  
172 are concluded with a list of the relevant references.

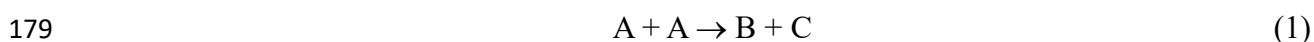
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## 174 **2.2 Conventions concerning rate coefficients**

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176 All of the reactions in the table are elementary processes. Thus the rate expression is derived  
177 from a statement of the reaction, e.g.

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$$181 \quad -\frac{1}{2} \frac{d[\text{A}]}{dt} = \frac{d[\text{B}]}{dt} = \frac{d[\text{C}]}{dt} = k[\text{A}]^2 \quad \text{Eq. (1)}$$

182

183 Note that the stoichiometric coefficient for A, i.e. 2, appears in the denominator before the rate  
184 of change of [A] (which is equal to  $2k[\text{A}]^2$ ) and as a power on the right-hand side.  
185 Representations of  $k$  as a function of temperature characterize simple “direct” bimolecular  
186 reactions. Sometimes it is found that  $k$  also depends on the pressure and the nature of the bath  
187 gas. This may be an indication of complex-formation during the course of the bimolecular  
188 reaction, which is always the case in combination reactions. In the following sections the  
189 representations of  $k$  which are adopted in these cases are explained.

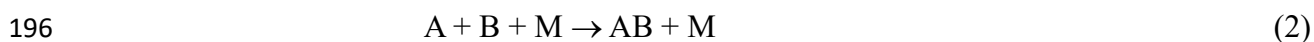
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## 191 **2.3 Treatment of combination and dissociation reactions**

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193 Unlike simple bimolecular reactions such as those considered in Sect. 2.2, combination  
194 reactions

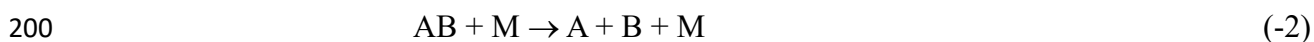
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198 and the reverse dissociation reactions

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202 are composed of sequences of different types of physical and chemical elementary processes.

203 Their rate coefficients reflect the more complicated sequential mechanism and depend on the

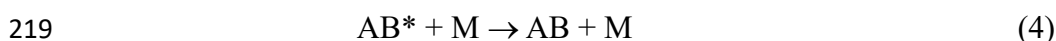
204 temperature,  $T$ , and the nature and concentration of the third body,  $M$ . In this evaluation, the  
 205 combination reactions are described by a formal second-order rate law:

$$206 \quad \frac{d[AB]}{dt} = k[A][B] \quad \text{Eq. (2)}$$

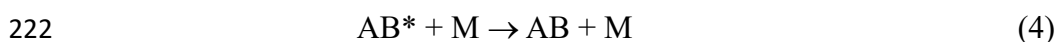
208 while dissociation reactions are described by a formal first-order rate law:

$$209 \quad \frac{-d[AB]}{dt} = k[AB] \quad \text{Eq. (3)}$$

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 211 In both cases,  $k$  depends on the temperature and on the concentration of  $M$ , i.e.,  $[M]$ . To  
 212 rationalize the representations of the rate coefficients used in this evaluation, we first consider  
 213 the Lindemann-Hinshelwood reaction scheme. The combination reactions follow an elementary  
 214 mechanism of the form,



218 while the dissociation reactions are characterized by:



222 Assuming quasi-stationary concentrations for the highly excited unstable species  $AB^*$  (i.e. that  
 223  $d[AB^*]/dt \approx 0$ ), it follows that the rate coefficient for the combination reaction is given by:

$$224 \quad k = k_3 \left( \frac{k_4[M]}{k_{-3} + k_4[M]} \right) \quad \text{Eq. (4)}$$

225 while that for the dissociation reaction is given by:

$$226 \quad k = k_{-4}[M] \left( \frac{k_{-3}}{k_{-3} + k_4[M]} \right) \quad \text{Eq. (5)}$$

227  
 228 In these equations the expressions before the parentheses represent the rate coefficients of the  
 229 process initiating the reaction, whereas the expressions within the parentheses denote the  
 230 fraction of reaction events which, after initiation, complete the reaction to products. In the low  
 231  
 232

236 pressure limit ( $[M] \rightarrow 0$ ) the rate coefficients are proportional to  $[M]$ ; in the high-pressure limit  
 237 ( $[M] \rightarrow \infty$ ) they are independent of  $[M]$ . It is useful to express  $k$  in terms of the limiting low  
 238 pressure and high-pressure rate coefficients,

$$240 \quad k_0 = \lim_{[M] \rightarrow 0} k([M]) \text{ and } k_\infty = \lim_{[M] \rightarrow \infty} k([M]) \quad \text{Eq. (6)}$$

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 243 From this convention, the Lindemann-Hinshelwood equation is obtained

$$245 \quad k = \frac{k_0 k_\infty}{k_0 + k_\infty} \quad \text{Eq. (7)}$$

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 247 It follows that, for combination reactions,  $k_0 = k_3 k_4 [M] / k_{-1}$  and  $k_\infty = k_3$ , while, for dissociation  
 248 reactions,  $k_0 = k_{-4} [M]$  and  $k_\infty = k_{-3} k_{-4} / k_4$ . Since detailed balancing applies, the ratio of the rate  
 249 coefficients for combination and dissociation at a fixed  $T$  and  $[M]$  is given by the equilibrium  
 250 constant  $K_c = k_3 k_4 / k_{-3} k_{-4}$ .

251 Starting from the high-pressure limit, the rate coefficients fall off with decreasing third body  
 252 concentration  $[M]$  and the corresponding representation of  $k$  as a function of  $[M]$  is termed the  
 253 “falloff curve” of the reaction. In practice, the above Lindemann-Hinshelwood expressions do  
 254 not suffice to characterize the falloff curves completely. Because of the multistep character of  
 255 the collisional deactivation ( $k_4 [M]$ ) and activation ( $k_{-4} [M]$ ) processes, and energy- and angular  
 256 momentum-dependences of the association ( $k_3$ ) and dissociation ( $k_{-3}$ ) steps, as well as other  
 257 phenomena, the falloff expressions have to be modified. This can be done by including a  
 258 broadening factor  $F$  to the Lindemann-Hinshelwood expression (Troe, 1979):

$$260 \quad k = \frac{k_0 k_\infty}{k_0 + k_\infty} F = k_0 \left( \frac{1}{1+x} \right) F = k_\infty \left( \frac{x}{1+x} \right) F \quad \text{Eq. (8)}$$

261  
 262 The broadening factor  $F$  depends on the ratio  $x = k_0/k_\infty$ , which is proportional to  $[M]$ , and can  
 263 be used as a measure of “reduced pressure”. The first factors on the right-hand side represent  
 264 the Lindemann-Hinshelwood expression and the additional broadening factor  $F$ , at not too high  
 265 temperatures, is approximately given by (Troe, 1979):

$$267 \quad \log F \cong \frac{\log F_c}{1 + [\log(k_0/k_\infty)/N]^2} \quad \text{Eq. (9)}$$

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where  $\log = \log_{10}$  and  $N \approx [0.75 - 1.27 \log F_c]$ .

When  $F_c$  decreases, the falloff curve broadens and becomes asymmetric (i.e.  $F(k_0/k_\infty) \neq F(k_\infty/k_0)$ ). The given equation for  $F$  then becomes insufficient and should be replaced, e.g. by

$$F(x) \approx (1+x)/(1+x^n)^{1/n} \quad \text{Eq. (10)}$$

where  $x = k_0/k_\infty$ ,  $n = [\ln 2 / \ln(2/F_c)] [0.8 + 0.2 x^q]$ ,  $q = (F_c - 1) / \ln(F_c/10)$  and  $\ln = \log_e$  (Troe and Ushakov, 2014). While the former equation for  $\log F$  appears acceptable as long as  $F_c \geq 0.6$ , the latter equation for  $F$  is more rigorous when  $F_c \leq 0.6$ . With these equations, falloff curves are represented in terms of the three parameters  $k_0$  (being proportional to  $[M]$ ),  $k_\infty$ , and  $F_c$ .

The parameters  $k_0$ ,  $k_\infty$ , and  $F_c$  depend on details of the intra- and intermolecular dynamics and in principle can be calculated. If the required information is not available, one has to obtain them by fitting experimental falloff curves with the expressions given above. Nevertheless, one may estimate  $F_c$  to be typically of the order of 0.49, 0.44, 0.39, and 0.35, if the reactants A and B in total have  $r = 3, 4, 5$ , and 6 external rotational degrees of freedom, respectively (Cobos and Troe, 2003; for the reaction  $\text{HO} + \text{NO}_2 + \text{M}$ , e.g. one would have  $r = 5$  and  $F_c \approx 0.39$ );  $F_c$  may be lower, if low frequency vibrations in A or B are relevant in addition to the rotations and if collisions are inefficient. Over the range 200 – 300 K often one can neglect a temperature dependence of  $F_c$  (for detailed calculations of  $F_c$ , including a dependence on the bath gas M, see e.g. Troe 1983; Troe and Ushakov, 2011, 2014). The accuracy of  $F(x)$  as given above is estimated to be about 10 percent. Larger differences between experimentally fitted  $F_c$  often are an indication for inadequate falloff extrapolations to  $k_0$  and/or  $k_\infty$ . In this case, the apparent values for  $k_0$ ,  $k_\infty$ , and  $F_c$  still can provide a satisfactory representation of the considered experimental data, in spite of the fact that  $k_0$  and/or  $k_\infty$  are not the real limiting values. If falloff curves are fitted in different ways, changes in  $F_c$  require changes in the limiting  $k_0$  and  $k_\infty$ . In the present evaluation, we generally follow the experimentally fitted values for  $k_0$ ,  $k_\infty$ , and  $F_c$ , provided that  $F_c$  does not differ too much from the standard values given above and theoretically modelled values. If large deviations are encountered, the experimental data are re-evaluated using  $F_c$ -values as given above. One should also note that  $k_\infty$  for combination reactions without a barrier often have only weak temperature dependences which in many cases can be neglected.

301 Besides the energy-transfer mechanism, i.e., reactions (3), (-3), and (4), a second mechanism  
302 may become relevant for some reactions considered here. This is the radical-complex (or  
303 chaperon) mechanism



307 which, in the low-pressure range, leads to  $k_0 = (k_5 / k_{-6})k_6 [M]$ . For some tri- and tetra-atomic  
308 adducts AB, e.g.,  $O + O_2 \rightarrow O_3$  and  $HO + C_6H_6 \rightarrow HOC_6H_6$ , the value of  $k_0$  may exceed that  
309 from the energy-transfer mechanism and show stronger temperature dependences (Luther et al.,  
310 2005; Teplukhin and Babikov, 2016). This mechanism may also influence high-pressure  
311 experiments when  $k_0$  from the radical-complex mechanism exceeds  $k_\infty$  from the energy-transfer  
312 mechanism (Oum et al., 2003). In this case falloff over wide pressure ranges cannot be  
313 represented by contributions from the energy-transfer mechanism alone, in particular when  
314 measurements at pressures above about 10 bar are taken into consideration.

315  
316 The dependence of  $k_0$  and  $k_\infty$  on the temperature  $T$  is represented in the form  $k \propto T^{-n}$  except for  
317 cases with an established energy barrier in the potential. We have used this form of temperature  
318 dependence because it usually gives a better fit to the data over a wider range of temperature  
319 than does the Arrhenius expression. It should be emphasised that the chosen form of the  
320 temperature dependence is often only adequate over limited temperature ranges such as 200–  
321 300 K. Obviously, the relevant values of  $n$  are different for  $k_0$  and  $k_\infty$ . In this evaluation, values  
322 of  $k_0$  are given for selected examples of third bodies M, and if possible for M = N<sub>2</sub>, O<sub>2</sub>, or air.

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## 324 **2.4 Treatment of complex-forming bimolecular reactions**

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326 Bimolecular reactions may follow the “direct” pathway

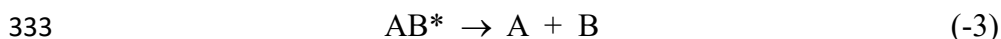
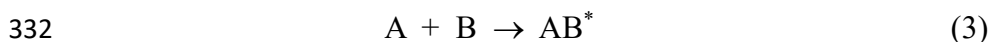
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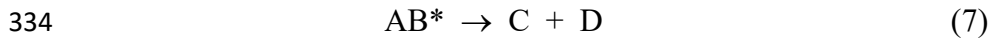


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330 and/or involve complex-formation, in the simplest way characterized by the steps

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337 (there may be additional pathways following from  $AB^*$ ; direct and complex-forming pathways  
 338 may or may not be coupled). Assuming quasi-stationary concentrations of  $AB^*$  (i.e. that  
 339  $d[AB^*]/dt \approx 0$  as in section 2.3), a Lindemann-Hinshelwood type analysis leads to

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341  $d[AB]/dt = k_{Ass} [A] [B]$  Eq. (11)

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343  $d[C]/dt = d[D]/dt = k_{CA} [A] [B]$  Eq. (12)

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345  $d[A]/dt = - ( k_{Ass} + k_{CA} ) [A] [B]$  Eq. (13)

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347 The rate constants for association ( $k_{Ass}$ ) and for chemical activation leading to product  
 348 formation ( $k_{CA}$ ) then are given by

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350  $k_{Ass} = k_1 k_2 [M] / ( k_{-1} + k_2 [M] + k_5 )$  Eq. (14)

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352  $k_{CA} = k_1 k_5 / ( k_{-1} + k_2 [M] + k_5 )$  Eq. (15)

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354 Note that  $k_{Ass}$  and  $k_{CA}$  are dependent on the nature and concentration of the third body M, in  
 355 addition to their temperature dependence. In reality, as for combination and dissociation  
 356 reactions, the given expressions for  $k_{Ass}$  and  $k_{CA}$  have to be extended by suitable broadening  
 357 factors  $F$  to account for the multistep character of processes (4) and the energy- and angular  
 358 momentum-dependences of processes (3), (-3), and (7). These broadening factors, however,  
 359 generally differ for  $k_{Ass}$  and  $k_{CA}$ ; also they generally differ from those of simple combination  
 360 reactions described in section 2.3. One should note that association and chemical activation  
 361 here are coupled such that their joint treatment is complicated. Some simplification is reached  
 362 when the processes first are treated separately and the coupling is introduced at the end (Troe,  
 363 2015). The corresponding rate constants of the separated processes are denoted by  $k_{Ass}^*$  and  
 364  $k_{CA}^*$  and are given by

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366  $k_{Ass}^* = k_3 k_4 [M] / ( k_{-3} + k_4 [M] )$  Eq. (16)

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and

$$k_{CA}^* = k_3 k_7 / (k_4 [M] + k_7). \quad \text{Eq. (17)}$$

$k_{Ass}^*$  then corresponds to the rate constant of a combination reaction described in section 2.3 and has a broadening factor  $F_{Ass}^*(x^*)$ .  $k_{CA}^*$  has to be treated in a different way and is expressed in the form

$$k_{CA}^* = k_{Ass,\infty} [ 1/ (1 + x^*) ] F_{CA}^*(x^*) \quad \text{Eq. (18)}$$

with  $x^* = k_{Ass,\infty} [M] / k_{CA,\infty}^*$  and a broadening factor  $F_{CA}^*(x)$  (Stewart et al., 1989). The latter factor is generally larger than  $F_{Ass}^*(x^*)$  (Troe, 2015). The rate parameters  $k_{CA,0}^*$  and  $k_{CA,\infty}^*$  depend on the molecular parameters and can be calculated theoretically or fitted experimentally (after the coupling between association and chemical activation has been accounted for). In practice one may try to represent the rate constants in the form of rate constants of separated processes  $k_{Ass}^*$  and  $k_{CA}^*$ . Coupling these rate constants then leads to a full representation of the rate constants in terms of the six rate parameters  $k_{Ass,0}$ ,  $k_{Ass,\infty}$ ,  $F_{Ass,c}$ ,  $k_{CA,0}$ ,  $k_{CA,\infty}$ , and  $F_{CA,c}$ . If one neglects the coupling and fits these parameters directly from the experiments (Miller and Klippenstein, 2001), however, one has to be aware of the fact that the values obtained do not correspond to those of separated, single-channel, association and chemical activation processes (for more details, see Troe, 2015).

As a consequence of the multistep character of complex-forming bimolecular reactions, a variety of temperature - and pressure - dependences of  $k_{Ass}$  and  $k_{CA}$  are observed. The low-pressure limit of the total rate constants  $k_{tot} = k_{Ass} + k_{CA}$ , i.e.,  $k_{tot,0} = k_{CA,0} = k_3 k_7 / (k_{-3} + k_7)$ , because of different energy - and angular momentum - dependences of the specific rate constants  $k_3$ ,  $k_{-3}$ , and  $k_7$ , may increase or decrease with temperature, the latter with the possibility to a change with an increase above a certain temperature.  $k_{tot}$ , as given above, may increase with pressure from  $k_{CA,0}$  to  $k_1$ , with  $M = H_2O$  often being a particularly efficient third body in the pressure - dependent range. The pressure dependence generally becomes less apparent with increasing temperature. Finally, the further fate of an addition product AB is of importance. It may be collisionally reactivated to energies where  $k_7 \gg k_{-3}$ , such that formation of  $C + D$  is enhanced

400 (in comparison to energies where  $k_7 \ll k_{-3}$ ). There is also the possibility that A-M (or B-M)  
401 complexes are formed which react in a chaperon mechanism with B (or A) and then form  
402 products. M = H<sub>2</sub>O here again may be particularly efficient. Without detailed theoretical  
403 analysis, in general, it will be difficult to disentangle the intrinsic mechanism. Therefore,  
404 reference to theoretical work is given for selected reactions.

405

## 406 **2.5 Photochemical reactions**

407

408 Tables are provided in the datasheets which summarise the available experimental data for: (i)  
409 absorption cross sections and (ii) quantum yields. These data are supplemented by a series of  
410 comments. The next table in each datasheet lists the preferred absorption cross section data and  
411 the preferred quantum yields at appropriate wavelength intervals. For absorption cross sections  
412 the intervals are usually 1 nm, 5 nm or 10 nm. Any temperature dependence of the absorption  
413 cross sections is also given where possible. The aim in presenting these preferred data is to  
414 provide a basis for calculating atmospheric photolysis rates. For absorption continua the  
415 temperature dependence is often represented by Sulzer-Wieland type expressions (Astholz et  
416 al., 1981). Alternately a simple empirical expression of the form:  $\log_{10}(\sigma_{T1} / \sigma_{T2}) = B*(T1-T2)$  is  
417 used. The comments again describe how the preferred data were selected and include other  
418 relevant points. The photochemical datasheets are concluded with a list of references.

419

## 420 **2.6 Conventions concerning absorption cross sections**

421

422 These are presented in the datasheets as “absorption cross sections per molecule, base e.” They  
423 are defined according to the equation:

424

$$425 \quad I / I_0 = \exp(-\sigma[N]l) \quad \text{Eq. (19)}$$

426

427 where  $I_0$  and  $I$  are the transmitted light intensities in the absence and presence of absorber,  $[N]$   
428 is the number concentration of absorber (expressed in molecule cm<sup>-3</sup>),  $l$  is the path length  
429 (expressed in cm), and  $\sigma$  is the absorption cross section (units of cm<sup>2</sup> molecule<sup>-1</sup>). Note that  
430 “molecule” is not a unit but is included here for clarity. Other definitions and units are frequently  
431 quoted. The closely related quantities “absorption coefficient” and “extinction coefficient” are  
432 often used, but care must be taken to avoid confusion in their definition, see Calvert (1990) for

433 definitions and discussion. It is always necessary to know the units of concentration and of path  
434 length and the type of logarithm (base e or base 10) corresponding to the definition. The decadic  
435 molar absorption coefficient,  $\epsilon$ , is often quoted, particularly in the older literature, and is defined  
436 as:

$$437 \quad \epsilon = \{1/([A]l)\} \log_{10}(I_0/I), \quad \text{Eq. (20)}$$

438 where  $[A]$  is the concentration of the absorber expressed in units of moles per liter. While  $\epsilon$  is  
439 often called an extinction coefficient, the term “extinction” should more properly be used for  
440 the sum of absorption and scattering. To convert from  $\epsilon$  (base 10, units of  $\text{dm}^3 \text{mol}^{-1} \text{cm}^{-1}$ ) to  $\sigma$   
441 (base e, units of  $\text{cm}^2 \text{molecule}^{-1}$ ) multiply by  $3.82 \times 10^{-20}$ .

442

## 443 **2.7 Assignment of uncertainties**

444

445 Under the heading “reliability,” estimates have been made of the absolute accuracies of the  
446 preferred values of  $k$  at 298 K and of the preferred values of  $E/R$  over the quoted temperature  
447 range. The accuracy of the preferred rate coefficient at 298 K is quoted as the term  $\Delta \log k$ ,  
448 where  $\Delta \log k = d$  and  $d$  is defined by the equation,  $\log k = c \pm d$ . This is equivalent to the  
449 statement that  $k$  is uncertain to a factor of  $f$ , where  $d = \log f$ . The accuracy of the preferred value  
450 of  $E/R$  is quoted as the term  $\Delta(E/R)$ , where  $\Delta(E/R) = g$  and  $g$  is defined by the equation  $E/R =$   
451  $h \pm g$ .  $d$  and  $g$  are uncertainties corresponding approximately to 95% confidence limits. For  
452 second-order rate coefficients listed in this evaluation, an estimate of the uncertainty at any  
453 given temperature within the recommended temperature range may be obtained from the  
454 equation:

455

$$456 \quad \Delta \log k(T) = \Delta \log k(298 \text{ K}) + 0.4343 \{ \Delta E/R(1/T - 1/298 \text{ K}) \} \quad \text{Eq. (21)}$$

457

458 The assignment of these absolute uncertainties in  $k$  and  $E/R$  is our subjective assessment.  
459 They are not determined by a rigorous, statistical analysis of the database, which is generally  
460 too limited to permit such an analysis. Rather, the uncertainties are based on our knowledge of  
461 the techniques, the difficulties of the experimental measurements, the potential for systematic  
462 errors, and the number of studies conducted and their agreement or lack thereof. Experience  
463 shows that for rate measurements of atomic and free radical reactions in the gas-phase, the  
464 precision of the measurement, i.e. the reproducibility, is usually good. Thus, for single studies  
465 of a particular reaction involving one technique, standard deviations, or even 95% confidence

466 limits, of  $\pm 10\%$  or less are frequently reported in the literature. Unfortunately, when we  
467 compare data for the same reaction studied by more than one group of investigators and  
468 involving different techniques, the rate coefficients sometimes differ by a factor of 2 or even  
469 more. This can only mean that one or more of the studies has large systematic errors which  
470 are difficult to detect. This is hardly surprising since it is not always possible to study atomic  
471 and free radical reactions in isolation, and consequently mechanistic and other difficulties  
472 frequently arise. Our assessment of uncertainty limits tends towards the cautious side. Our  
473 assessment of uncertainties in the preferred values are not determined by a rigorous, statistical  
474 analysis of the database, which is generally too limited to permit such an analysis. Rather, the  
475 uncertainties are based on our knowledge of the techniques, the difficulties of the  
476 experimental measurements, the potential for systematic errors, and the number of studies  
477 conducted and their agreement or lack thereof.

478  
479 **Author contribution:** All authors defined the scope of the work. TJW, JNC, and AM developed  
480 and drafted the datasheets and manuscript. All authors reviewed, refined, and revised the  
481 manuscript and datasheets.

482  
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494  
495  
496

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620

621 **Table 1 Summary of recommended rate coefficients<sup>a</sup> for organic halogen reactions added since publication**  
 622 **of Volume IV**

Datasheet ID <sup>b</sup>	Reaction	$k_{298} / \text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$	$\Delta \log k_{298}^a$ <sup>c</sup>	$k(T) / \text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$	Temp. range/K	$\Delta(E/R) / \text{K}^c$
<i>Organic FOx, ClOx, BrOx, and IOx reactions added to the IUPAC website (see Supplementary Material for datasheets)</i>						
<i>Halogenated alkanes</i>						
oFOx72	HO + CF <sub>3</sub> CH <sub>2</sub> CH <sub>3</sub> (HFC-263fb) → products	$4.9 \times 10^{-14}$	0.15	$3.7 \times 10^{-12} \exp(-1290/T)$	240-370	300
oFOx73	HO + CF <sub>3</sub> CHFCH <sub>2</sub> F (HFC-245eb) → products	$1.6 \times 10^{-14}$	0.15	$1.1 \times 10^{-11} \exp(-1250/T)$	240-380	300
oFOx74	HO + CHF <sub>2</sub> CHFCHF <sub>2</sub> (HFC-245ea) → products	$1.8 \times 10^{-14}$	0.15	$1.8 \times 10^{-12} \exp(-1375/T)$	240-380	300
oFOx75	HO + CF <sub>3</sub> CH <sub>2</sub> CHF <sub>2</sub> (HFC-245fa) → products	$6.9 \times 10^{-15}$	0.12	$6.0 \times 10^{-13} \exp(-1331/T)$	270-370	300
oFOx76	HO + CF <sub>3</sub> CH <sub>2</sub> CF <sub>2</sub> CH <sub>3</sub> (HFC-365mfc) → products	$7.1 \times 10^{-15}$	0.20	$1.6 \times 10^{-12} \exp(-1620/T)$	270-380	200
oFOx77	HO + CF <sub>3</sub> CH <sub>2</sub> CH <sub>2</sub> CF <sub>3</sub> (HFC-356mff) → products	$7.8 \times 10^{-15}$	0.10	$2.6 \times 10^{-12} \exp(-1734/T)$	260-370	300
oFOx78	HO + CF <sub>3</sub> CF <sub>2</sub> CH <sub>2</sub> CH <sub>2</sub> F (HFC-356mcf) → products	$4.2 \times 10^{-14}$	0.15	$1.7 \times 10^{-12} \exp(-1108/T)$	250-370	300
oFOx79	HO + CHF <sub>2</sub> CF <sub>2</sub> CF <sub>2</sub> CHF <sub>2</sub> (HFC-338pcc) → products	$4.3 \times 10^{-15}$	0.08	$7.82 \times 10^{-13} \exp(-1548/T)$	230-420	200
oFOx80	HO + CF <sub>3</sub> CH <sub>2</sub> CF <sub>2</sub> CH <sub>2</sub> CF <sub>3</sub> (HFC-458mfef) → products	$2.6 \times 10^{-15}$	0.15	$1.23 \times 10^{-12} \exp(-1833/T)$	270-360	300
oFOx81	HO + CF <sub>3</sub> CHFCHF <sub>2</sub> CF <sub>2</sub> CF <sub>3</sub> (HFC-44-10mee) → products	$3.3 \times 10^{-15}$	0.12	$5.68 \times 10^{-13} \exp(-1534/T)$	240-400	300
oFOx82	HO + CF <sub>3</sub> CF <sub>2</sub> CH <sub>2</sub> CH <sub>2</sub> CF <sub>2</sub> CF <sub>3</sub> (HFC-55-10mcf) → products	$8.3 \times 10^{-15}$	0.20			
oFOx83	HO + CHF <sub>2</sub> (CF <sub>3</sub> ) <sub>4</sub> CF <sub>3</sub> (HFC-52-13p) → products	$1.8 \times 10^{-15}$	0.10	$5.76 \times 10^{-13} \exp(-1726/T)$	250-430	300
oClOx86	HO + C <sub>2</sub> H <sub>5</sub> Cl → products	$3.7 \times 10^{-13}$	0.10	$4.25 \times 10^{-12} \exp(-727/T)$	220-400	200
oClOx87	HO + CH <sub>2</sub> ClCH <sub>2</sub> Cl → products	$2.4 \times 10^{-13}$	0.08	$8.69 \times 10^{-12} \exp(-1070/T)$	290-360	200
oClOx88	HO + CH <sub>3</sub> CHCl <sub>2</sub> → products	$2.76 \times 10^{-13}$	0.10	$2.04 \times 10^{-12} \exp(-596/T)$	290-370	300
oBrOx16	HO + CHBr <sub>3</sub> → products	$2.7 \times 10^{-13}$	0.15	$1.0 \times 10^{-12} \exp(-388/T)$	290-370	300
oBrOx17	HO + C <sub>2</sub> H <sub>5</sub> Br → products	$3.3 \times 10^{-13}$	0.15	$2.25 \times 10^{-12} \exp(-576/T)$	230-300	300
oBrOx18	HO + CH <sub>2</sub> BrCH <sub>2</sub> Br → products	$2.22 \times 10^{-13}$	0.10	$7.69 \times 10^{-12} \exp(-1056/T)$	290-370	300
oBrOx19	HO + <i>n</i> -C <sub>3</sub> H <sub>7</sub> Br → products	$1.0 \times 10^{-12}$	0.10	$3.91 \times 10^{-12} \exp(-399/T)$	210-300	300
oBrOx20	HO + CH <sub>3</sub> CHBrCH <sub>3</sub> → products	$7.58 \times 10^{-13}$	0.06	$1.96 \times 10^{-12} \exp(-283/T)$	210-355	200
oBrOx21	HO + <i>n</i> -C <sub>4</sub> H <sub>9</sub> Br → products	$2.3 \times 10^{-12}$	0.20			
oBrOx22	HO + <i>n</i> -C <sub>5</sub> H <sub>11</sub> Br → products	$3.7 \times 10^{-12}$	0.20			
oBrOx23	HO + <i>n</i> -C <sub>6</sub> H <sub>13</sub> Br → products	$5.5 \times 10^{-12}$	0.20			
oIOx4	HO + CH <sub>3</sub> CH <sub>2</sub> I → products	$3.43 \times 10^{-13}$	0.10	$5.55 \times 10^{-12} \exp(-830/T)$	290-380	200
oIOx5	HO + CH <sub>3</sub> CH <sub>2</sub> CH <sub>2</sub> I → products	$1.36 \times 10^{-12}$	0.08	$1.86 \times 10^{-11} \exp(-780/T)$	290-380	200
oIOx6	HO + CH <sub>3</sub> CHICH <sub>3</sub> → products	$1.29 \times 10^{-12}$	0.08	$7.64 \times 10^{-11} \exp(-530/T)$	290-380	200
oFOx108	Cl + CHF <sub>2</sub> CH <sub>2</sub> CF <sub>3</sub> (HFC-245fa) → products	$6.9 \times 10^{-15}$	0.30			
oFOx110	Cl + CF <sub>3</sub> CHF <sub>2</sub> CF <sub>3</sub> (HFC-227ea) → products	$4.4 \times 10^{-16}$	0.15			
oFOx111	Cl + CHF <sub>3</sub> (HFC-23) → products	$3.4 \times 10^{-18}$	0.50			
oBrOx24	Cl + CH <sub>3</sub> Br → products	$4.5 \times 10^{-13}$	0.05	$1.38 \times 10^{-11} \exp(-1020/T)$	210-300	100
<i>Halogenated alkenes</i>						
oFOx112	HO + CF <sub>2</sub> =CF <sub>2</sub> (HFO-1114) → products	$1.04 \times 10^{-11}$	0.06	$3.84 \times 10^{-12} \exp(297/T)$	250-500	100
oFOx114	HO + CF <sub>3</sub> CF=CH <sub>2</sub> (HFO-1234yf) → products	$1.12 \times 10^{-11}$	0.06	$1.16 \times 10^{-12} \exp(-10/T)$	200-300	100
oFOx115	HO + <i>E</i> -CF <sub>3</sub> CH=CHF (HFO-1234ze(E)) → products	$7.07 \times 10^{-13}$	0.06	$6.91 \times 10^{-13} \exp(7/T)$	210-300	100
oFOx117	HO + <i>Z</i> -CF <sub>3</sub> CH=CHF (HFO-1234ze(Z)) → products	$1.21 \times 10^{-12}$	0.15	$8.46 \times 10^{-13} \exp(106/T)$	260-300	100
oFOx118	HO + <i>E</i> -CF <sub>3</sub> CF=CHF (HFO-1225ze(E)) → products	$2.2 \times 10^{-12}$	0.15			
oFOx119	HO + <i>Z</i> -CF <sub>3</sub> CF=CHF (HFO-1225ze(Z)) → products	$1.2 \times 10^{-12}$	0.10	$7.60 \times 10^{-13} \exp(155/T)$	200-300	100
oFOx116	HO + CF <sub>3</sub> CF <sub>2</sub> =CF <sub>2</sub> (FO-1216) → products	$2.18 \times 10^{-12}$	0.04	$7.38 \times 10^{-13} \exp(322/T)$	240-340	100
oFOx135	HO + <i>E</i> -CF <sub>3</sub> CH=CHCF <sub>3</sub> (HFO-1336mzz(E)) → products	$1.31 \times 10^{-13}$	0.06	$6.94 \times 10^{-13} \exp(-496/T)$	210-380	100
oFOx136	HO + <i>Z</i> -CF <sub>3</sub> CH=CHCF <sub>3</sub> (HFO-1336mzz(Z)) → products	$4.80 \times 10^{-13}$	0.06	$2.46 \times 10^{-13} \exp(199/T)$	210-300	100
oClOx95	HO + CH <sub>2</sub> =CHCl (vinyl chloride) → products	$7.55 \times 10^{-12}$	0.08	$2.54 \times 10^{-12} \exp(325/T)$	280-600	100
oFOx120	HO + <i>E</i> -CF <sub>3</sub> CH=CHCl (HCFO-1233zd(E)) → products	$3.53 \times 10^{-13}$	0.06	$8.79 \times 10^{-13} \exp(-272/T)$	220-300	100
oFOx121	HO + <i>Z</i> -CF <sub>3</sub> CH=CHCl (HCFO-1233zd(Z)) → products	$9.24 \times 10^{-13}$	0.06	$3.61 \times 10^{-13} \exp(280/T)$	220-300	100
oFOx165	HO + <i>E</i> -CF <sub>3</sub> CF=CHCl (HCFO-1224yd(E)) → products	$1.30 \times 10^{-12}$	0.08	$1.09 \times 10^{-12} \exp(53/T)$	250-430	100
oFOx166	HO + <i>Z</i> -CF <sub>3</sub> CF=CHCl (HCFO-1224yd(Z)) → products	$5.83 \times 10^{-13}$	0.08	$8.03 \times 10^{-13} \exp(-95/T)$	250-430	100

oFOx164	HO + <i>E</i> -CF <sub>3</sub> CBr=CH <sub>2</sub> (HBFO-1233xfB) → products	3.84 × 10 <sup>-12</sup>	0.06	1.11 × 10 <sup>-12</sup> exp(370/ <i>T</i> )	250-430	100
oFOx154	NO <sub>3</sub> + CF <sub>2</sub> =CF <sub>2</sub> (HFO-1114) → products	< 3 × 10 <sup>-15</sup>				
oFOx153	NO <sub>3</sub> + CF <sub>3</sub> CF <sub>2</sub> =CH <sub>2</sub> (HFO-1234yf) → products	2.6 × 10 <sup>-17</sup>	0.15			
oFOx122	NO <sub>3</sub> + <i>Z</i> -CF <sub>3</sub> CF=CHF (HFO-1225ye(Z)) → products	4.2 × 10 <sup>-18</sup>	0.20			
oFOx123	NO <sub>3</sub> + CF <sub>3</sub> CF <sub>2</sub> =CF <sub>2</sub> (FO-1216) → products	< 3 × 10 <sup>-15</sup>				
oFOx155	NO <sub>3</sub> + CF <sub>2</sub> =CF <sub>2</sub> CF=CF <sub>2</sub> → products	1.56 × 10 <sup>-15</sup>	0.15			
oClOx96	NO <sub>3</sub> + CH <sub>2</sub> =CHCl (vinyl chloride) → products	4.6 × 10 <sup>-16</sup>	0.10	1.8 × 10 <sup>-13</sup> exp(-1780/ <i>T</i> )	260-380	300
oFOx126	O <sub>3</sub> + CF <sub>2</sub> =CF <sub>2</sub> (HFO-1114) → products	4.8 × 10 <sup>-21</sup>	0.15			
oFOx113	O <sub>3</sub> + CF <sub>3</sub> CH=CH <sub>2</sub> (HFO-1243zf) → products	1.43 × 10 <sup>-20</sup>	0.08	4.65 × 10 <sup>-16</sup> exp(-3096/ <i>T</i> )	290-390	200
oFOx128	O <sub>3</sub> + CF <sub>3</sub> CF=CH <sub>2</sub> (HFO-1234yf) → products	2.67 × 10 <sup>-21</sup>	0.08			
oFOx129	O <sub>3</sub> + <i>E</i> -CF <sub>3</sub> CH=CHF (HFO-1234ze(E)) → products	2.50 × 10 <sup>-21</sup>	0.10			
oFOx156	O <sub>3</sub> + <i>Z</i> -CF <sub>3</sub> CH=CHF (HFO-1234ze(Z)) → products	1.7 × 10 <sup>-21</sup>	0.15			
oFOx130	O <sub>3</sub> + CF <sub>3</sub> CF <sub>2</sub> =CF <sub>2</sub> (FO-1216) → products	6.2 × 10 <sup>-22</sup>	0.30			
oFOx157	O <sub>3</sub> + CF <sub>2</sub> =CF <sub>2</sub> CF=CF <sub>2</sub> → products	7.9 × 10 <sup>-21</sup>	0.15	9.51 × 10 <sup>-17</sup> exp(-2800/ <i>T</i> )	220-320	200
oFOx127	O <sub>3</sub> + <i>E</i> -CF <sub>3</sub> CH=CHCF <sub>3</sub> (HFO-1336mzz(E)) → products	4.14 × 10 <sup>-22</sup>	0.10			
oFOx124	O <sub>3</sub> + <i>Z</i> -CF <sub>3</sub> CH=CHCF <sub>3</sub> (HFO-1336mzz(Z)) → products	7.09 × 10 <sup>-22</sup>	0.08			
oClOx97	O <sub>3</sub> + CH <sub>2</sub> =CHCl (vinyl chloride) → products	2.5 × 10 <sup>-19</sup>	0.15			
oFOx132	O <sub>3</sub> + <i>E</i> -CF <sub>3</sub> CH=CHCl (HCFO-1233zd(E)) → products	1.51 × 10 <sup>-21</sup>	0.15			
oFOx131	O <sub>3</sub> + <i>Z</i> -CF <sub>3</sub> CH=CHCl (HCFO-1233zd(Z)) → products	1.53 × 10 <sup>-21</sup>	0.15			
oFOx125	O <sub>3</sub> + CF <sub>3</sub> CCl=CH <sub>2</sub> (HCFO-1233xf) → products	3.00 × 10 <sup>-21</sup>	0.08			
<b>Halogenated alcohols</b>						
oFOx84	HO + CH <sub>2</sub> FCH <sub>2</sub> OH → products	9.12 × 10 <sup>-13</sup>	0.08	2.23 × 10 <sup>-12</sup> exp(-266/ <i>T</i> )	230-300	200
oFOx85	HO + CHF <sub>2</sub> CH <sub>2</sub> OH → products	2.61 × 10 <sup>-13</sup>	0.08	1.63 × 10 <sup>-12</sup> exp(-545/ <i>T</i> )	220-300	200
oFOx86	HO + CF <sub>3</sub> CH <sub>2</sub> OH → products	1.00 × 10 <sup>-13</sup>	0.06	1.25 × 10 <sup>-12</sup> exp(-754/ <i>T</i> )	220-300	100
oFOx87	HO + CF <sub>3</sub> CH <sub>2</sub> CH <sub>2</sub> OH → products	9.6 × 10 <sup>-13</sup>	0.10	2.72 × 10 <sup>-12</sup> exp(-305/ <i>T</i> )	260-360	100
oFOx88	HO + C <sub>2</sub> F <sub>5</sub> CH <sub>2</sub> OH → products	1.05 × 10 <sup>-13</sup>	0.06	1.28 × 10 <sup>-12</sup> exp(-748/ <i>T</i> )	250-430	200
oFOx89	HO + CF <sub>3</sub> CH(OH)CF <sub>3</sub> → products	2.43 × 10 <sup>-14</sup>	0.12	3.94 × 10 <sup>-15</sup> ( <i>T</i> /298) <sup>4.57</sup> exp(542/ <i>T</i> )	250-430	
oFOx158	HO + (CF <sub>3</sub> ) <sub>2</sub> C(OH)CH <sub>3</sub> → products	7.71 × 10 <sup>-15</sup>	0.12	1.90 × 10 <sup>-18</sup> ( <i>T</i> /298) <sup>11.5</sup> exp(2476/ <i>T</i> )	230-370	
oFOx159	HO + (CF <sub>3</sub> ) <sub>3</sub> COH → products	8.6 × 10 <sup>-16</sup>	0.12	3.0 × 10 <sup>-20</sup> ( <i>T</i> /298) <sup>11.3</sup> exp(3060/ <i>T</i> )	230-370	
oFOx90	HO + CF <sub>3</sub> CHFCF <sub>2</sub> CH <sub>2</sub> OH → products	1.3 × 10 <sup>-13</sup>	0.12	2.26 × 10 <sup>-12</sup> exp(-848/ <i>T</i> )	250-430	200
oFOx91	HO + <i>n</i> -C <sub>3</sub> F <sub>7</sub> CH <sub>2</sub> OH → products	1.11 × 10 <sup>-13</sup>	0.10	6.06 × 10 <sup>-12</sup> exp(-1192/ <i>T</i> )	280-370	200
oFOx92	HO + <i>n</i> -C <sub>4</sub> F <sub>9</sub> CH <sub>2</sub> OH → products	9.4 × 10 <sup>-14</sup>	0.15			
oFOx93	HO + <i>n</i> -C <sub>4</sub> F <sub>9</sub> CH <sub>2</sub> CH <sub>2</sub> OH → products	1.0 × 10 <sup>-12</sup>	0.15			
oFOx94	HO + <i>n</i> -C <sub>6</sub> F <sub>13</sub> CH <sub>2</sub> CH <sub>2</sub> OH → products	8.3 × 10 <sup>-13</sup>	0.15			
oFOx95	HO + <i>n</i> -C <sub>8</sub> F <sub>17</sub> CH <sub>2</sub> CH <sub>2</sub> OH → products	9.2 × 10 <sup>-13</sup>	0.15			
oFOx96	HO + CF <sub>3</sub> CH(OH) <sub>2</sub> → products	1.2 × 10 <sup>-13</sup>	0.20			
oClOx90	HO + CH <sub>2</sub> ClCH <sub>2</sub> OH → products	1.3 × 10 <sup>-12</sup>	0.20			
oClOx91	HO + CCl <sub>3</sub> CH <sub>2</sub> OH → products	2.5 × 10 <sup>-13</sup>	0.20			
<b>Halogenated aldehydes</b>						
oFOx97	HO + CHF <sub>2</sub> CHO → products	1.6 × 10 <sup>-12</sup>	0.15			
oFOx98	HO + C <sub>2</sub> F <sub>5</sub> CHO → products	5.2 × 10 <sup>-13</sup>	0.10	2.42 × 10 <sup>-12</sup> exp(-458/ <i>T</i> )	250-360	200
oFOx99	HO + <i>n</i> -C <sub>3</sub> F <sub>7</sub> CHO → products	5.8 × 10 <sup>-13</sup>	0.08	2.0 × 10 <sup>-12</sup> exp(-369/ <i>T</i> )	250-380	200
oFOx100	HO + <i>n</i> -C <sub>4</sub> F <sub>9</sub> CHO → products	6.1 × 10 <sup>-13</sup>	0.08	2.0 × 10 <sup>-12</sup> exp(-356/ <i>T</i> )	250-380	150
oFOx101	HO + CF <sub>3</sub> CH <sub>2</sub> CHO → products	2.7 × 10 <sup>-12</sup>	0.15	7.74 × 10 <sup>-12</sup> exp(-314/ <i>T</i> )	260-360	150
oFOx102	HO + <i>n</i> -C <sub>6</sub> F <sub>13</sub> CH <sub>2</sub> CHO → products	2.0 × 10 <sup>-12</sup>	0.15			
oFOx103	HO + <i>n</i> -C <sub>8</sub> F <sub>17</sub> CH <sub>2</sub> CHO → products	1.8 × 10 <sup>-12</sup>	0.15			
<b>Halogenated ketones</b>						
oFOx104	HO + C <sub>2</sub> F <sub>5</sub> C(O)CF(CF <sub>3</sub> ) <sub>2</sub> → products	< 5 × 10 <sup>-16</sup>				
oClOx92	HO + CH <sub>2</sub> ClC(O)CH <sub>3</sub> → products	4.4 × 10 <sup>-13</sup>	0.15			
oClOx93	HO + CHCl <sub>2</sub> C(O)CH <sub>3</sub> → products	4.0 × 10 <sup>-13</sup>	0.15			
oClOx94	HO + CCl <sub>3</sub> C(O)CH <sub>3</sub> → products	1.5 × 10 <sup>-14</sup>	0.15			
<b>Halogenated acids</b>						
oFOx105	HO + C <sub>2</sub> F <sub>5</sub> C(O)OH → products	1.55 × 10 <sup>-13</sup>	0.15			
oFOx106	HO + <i>n</i> -C <sub>3</sub> F <sub>7</sub> C(O)OH → products	1.55 × 10 <sup>-13</sup>	0.15			

oFOx107	HO + <i>n</i> -C <sub>4</sub> F <sub>9</sub> C(O)OH → products	1.55 × 10 <sup>-13</sup>	0.15			
<b>Halogenated ethers</b>						
oFOx137	HO + CH <sub>3</sub> OCHF <sub>2</sub> → products	3.52 × 10 <sup>-14</sup>	0.15	1.16 × 10 <sup>-11</sup> exp(-1728/ <i>T</i> )	290-470	100
oFOx138	HO + CH <sub>3</sub> OCF <sub>3</sub> → products	1.29 × 10 <sup>-14</sup>	0.10	1.10 × 10 <sup>-12</sup> exp(-1324/ <i>T</i> )	290-470	100
oFOx139	HO + CHF <sub>2</sub> OCHF <sub>2</sub> → products	2.20 × 10 <sup>-15</sup>	0.10	1.04 × 10 <sup>-12</sup> exp(-1836/ <i>T</i> )	270-470	100
oFOx140	HO + CHF <sub>2</sub> OCF <sub>3</sub> → products	4.57 × 10 <sup>-16</sup>	0.10	3.09 × 10 <sup>-13</sup> exp(-1942/ <i>T</i> )	290-400	100
oFOx141	HO + CH <sub>3</sub> OCHF <sub>2</sub> CF <sub>3</sub> → products	1.57 × 10 <sup>-13</sup>	0.10	1.74 × 10 <sup>-12</sup> exp(-716/ <i>T</i> )	250-330	100
oFOx142	HO + CH <sub>3</sub> OCF <sub>2</sub> CHF <sub>2</sub> → products	2.24 × 10 <sup>-14</sup>	0.10	2.50 × 10 <sup>-12</sup> exp(-1405/ <i>T</i> )	240-440	100
oFOx143	HO + CH <sub>3</sub> OCH <sub>2</sub> CF <sub>3</sub> → products	6.56 × 10 <sup>-13</sup>	0.10	3.61 × 10 <sup>-12</sup> exp(-508/ <i>T</i> )	260-360	300
oFOx144	HO + CH <sub>3</sub> OC <sub>2</sub> F <sub>5</sub> → products	1.20 × 10 <sup>-14</sup>	0.10	1.84 × 10 <sup>-12</sup> exp(-1499/ <i>T</i> )	240-440	100
oFOx145	HO + <i>n</i> -C <sub>3</sub> F <sub>7</sub> OCH <sub>3</sub> → products	1.18 × 10 <sup>-14</sup>	0.10	1.98 × 10 <sup>-12</sup> exp(-1526/ <i>T</i> )	240-440	100
oFOx146	HO + <i>i</i> -C <sub>3</sub> F <sub>7</sub> OCH <sub>3</sub> → products	1.52 × 10 <sup>-14</sup>	0.10	1.86 × 10 <sup>-12</sup> exp(-1432/ <i>T</i> )	240-440	100
oFOx147	HO + C <sub>4</sub> F <sub>9</sub> OCH <sub>3</sub> → products	1.19 × 10 <sup>-14</sup>	0.08	1.15 × 10 <sup>-12</sup> exp(-1362/ <i>T</i> )	250-330	100
oFOx148	HO + CH <sub>3</sub> OCH(CF <sub>3</sub> ) <sub>2</sub> → products	2.29 × 10 <sup>-13</sup>	0.10	1.08 × 10 <sup>-12</sup> exp(-461/ <i>T</i> )	230-340	100
oFOx149	HO + CH <sub>2</sub> FOCH(CF <sub>3</sub> ) <sub>2</sub> (Sevoflurane) → products	4.14 × 10 <sup>-14</sup>	0.10	1.24 × 10 <sup>-12</sup> exp(-1017/ <i>T</i> )	230-440	200
oFOx150	HO + CHF <sub>2</sub> OCHFCF <sub>3</sub> (Desflurane) → products	4.08 × 10 <sup>-15</sup>	0.10	7.43 × 10 <sup>-13</sup> exp(-1551/ <i>T</i> )	230-300	200
<b>Halogenated vinyl ethers</b>						
oFOx133	HO + CF <sub>3</sub> OCF=CF <sub>2</sub> → products	2.96 × 10 <sup>-12</sup>	0.10	1.01 × 10 <sup>-12</sup> exp(320/ <i>T</i> )	250-430	100
oFOx134	HO + C <sub>2</sub> F <sub>5</sub> OCF=CF <sub>2</sub> → products	3.0 × 10 <sup>-12</sup>	0.10	6.0 × 10 <sup>-13</sup> exp(480/ <i>T</i> )	200-300	100
<b>Peroxy radicals</b>						
oFOx160	CF <sub>3</sub> C(O)O <sub>2</sub> + HO <sub>2</sub> → CF <sub>3</sub> C(O)OOH + O <sub>2</sub> (1)	<i>k</i> <sub>1</sub> / <i>k</i> = 1.8 × 10 <sup>-12</sup>				
	→ CF <sub>3</sub> C(O)OH + O <sub>3</sub> (2)	<i>k</i> <sub>2</sub> / <i>k</i> = 7.6 × 10 <sup>-12</sup>				
	→ CF <sub>3</sub> C(O)O + HO (3)	<i>k</i> <sub>3</sub> / <i>k</i> = 1.12 × 10 <sup>-11</sup>				
	Overall	2.0 × 10 <sup>-11</sup>	0.3			
oFOx161	CF <sub>3</sub> C(O)O <sub>2</sub> + NO → CF <sub>3</sub> C(O)O + NO <sub>2</sub>	2.8 × 10 <sup>-11</sup>	0.2	4.0 × 10 <sup>-12</sup> exp(560/ <i>T</i> )	220-340	200
oFOx162	CF <sub>3</sub> C(O)O <sub>2</sub> + NO <sub>2</sub> + M → CF <sub>3</sub> C(O)O <sub>2</sub> NO <sub>2</sub> + M	6.6 × 10 <sup>-12</sup>	0.3			
oFOx163	CF <sub>3</sub> C(O)O <sub>2</sub> NO <sub>2</sub> + M → CF <sub>3</sub> C(O)O <sub>2</sub> + NO <sub>2</sub> + M	5.0 × 10 <sup>-20</sup>		5.0 × 10 <sup>-2</sup> exp(-12350/ <i>T</i> )	290-330	
		[N <sub>2</sub> ] ( <i>k</i> <sub>0</sub> / <i>s</i> <sup>-1</sup> )		1.1 × 10 <sup>17</sup> exp(-14440/ <i>T</i> )		
		( <i>k</i> <sub>2</sub> / <i>s</i> <sup>-1</sup> )				
		7.95 × 10 <sup>-5</sup> (1 bar) <i>k</i> / <i>s</i> <sup>-1</sup>				
<b>Photochemical reactions added to the IUPAC website (see Supplementary Material for datasheets)</b>						
PF5	CHF <sub>2</sub> CHO + <i>hν</i> → products					
PF6	C <sub>2</sub> F <sub>5</sub> CHO + <i>hν</i> → products					
PF7	<i>n</i> -C <sub>3</sub> F <sub>7</sub> CHO + <i>hν</i> → products					
PF8	<i>n</i> -C <sub>4</sub> F <sub>9</sub> CHO + <i>hν</i> → products					
PF9	CF <sub>3</sub> CH <sub>2</sub> CHO + <i>hν</i> → products					
PF10	<i>n</i> -C <sub>6</sub> F <sub>13</sub> CH <sub>2</sub> CHO + <i>hν</i> → products					

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624 a: Rate coefficients are also known as rate constants, both terms are used here.

625 b: See corresponding datasheets in Supplement for further information (e.g., methods used and products formed).

626 c: The cited uncertainty is an expanded uncertainty corresponding approximately to a 95% confidence limit.

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