



25 to mobile colloids, decreased from about 0.09–0.14 at low velocity ($\sim 0.004 \text{ cm s}^{-1}$) to about
26 0.03–0.04 at high velocity ($\sim 0.03 \text{ cm s}^{-1}$). In addition, γ was generally higher in 10 cm
27 columns than in 30 cm columns, especially at low velocity. Flow simulations further
28 suggested that increasing velocity reduced the dominance of low-velocity regions and
29 enhanced the continuity of active flow pathways. These results indicate that γ is not a fixed
30 geometric constant, but a flow-dependent effective parameter governed by pore
31 accessibility and transport conditions.

32 **Keywords:** Size exclusion effect, colloids transport, porosity, NMR, μ -CT

33



34 **1 Introduction**

35 Colloid transport in porous media is a complex yet critical phenomenon, particularly
36 in environmental contexts such as groundwater contamination, where it strongly influences
37 pollutant fate (Akbulut and Min, 2025; Akdogan and Guven, 2019; Bradford et al., 2013).
38 A key mechanism underlying this process is that colloids are often transported faster than
39 dissolved tracers, a phenomenon attributed to the size exclusion effect (SEE). SEE arises
40 because colloids, owing to their finite dimensions, are unable to access the entire pore
41 volume available to solutes or water molecules (Donath et al., 2019).

42 Quantitative characterization of pore structures provides a critical basis for evaluating
43 SEE. The occurrence and strength of SEE are primarily governed by the geometry of pore
44 spaces and the relative size of colloids to pore throats (Auset and Keller, 2004; Chakraborty
45 et al., 2024). Micromodel experiments provide direct visual insights into the relationship
46 between colloids and pore-throat sizes at a microscopic scale. For instance,
47 Sirivithayapakorn and Keller (2003) demonstrated that colloids can only enter pore throats
48 larger than ~ 1.5 times their diameter. At the column scale, however, recent studies have
49 revealed a significant negative linear correlation between the fraction of the water-saturated
50 pore volume inaccessible to mobile colloids (γ) and the median grain size of the porous
51 medium (d_{50}) (Wang et al., 2024). While this correlation suggests a link between the bulk
52 properties of the medium and the extent of SEE, it is an indirect relationship based on the
53 average properties of the entire medium rather than the pores.

54 Noninvasive techniques such as nuclear magnetic resonance (NMR) and micro-
55 computed tomography (μ -CT) have become mainstream tools for pore structure
56 characterization (Shen et al., 2025; Xiao et al., 2016; Zhao et al., 2017). NMR infers pore



57 size distributions and fluid dynamics from relaxation times (T_2 or T_1-T_2) (Morales-Chávez
58 et al., 2025). It is particularly well-suited for nanoscale characterization, though calibration
59 is required to account for surface relaxation effects. In contrast, μ -CT yields high-resolution
60 3D images of pore geometry and connectivity at the micrometer scale. However, it typically
61 cannot resolve sub-micron pores (Adhikari et al., 2016). The integration of NMR and μ -
62 CT has emerged as a powerful approach, as the two methods complement each other to
63 provide a multi-scale, high-precision understanding of the pore network structure. Recent
64 advances include finite-element-based NMR modeling to simulate signals for the accurate
65 pore size distribution analysis, as well as NMR-CT data registration approaches that
66 optimize experimental design to determine surface relaxivity (ρ) and predict permeability
67 across scales (Shen et al., 2025; Xiao et al., 2016; Zhao et al., 2017).

68 In addition to pore structure, flow velocity exerts a profound influence on SEE. Some
69 studies show that increased flow velocities can mitigate SEE. Bai et al. (2015) found that
70 the early breakthrough of colloids decreased as the flow rate increased in their infiltration
71 experiments. Similarly, Massei et al. (2002) observed that with increasing Darcy velocity,
72 colloids showed reduced early breakthrough, with the effect disappearing at velocities over
73 0.073 cm s^{-1} . They attributed this to changes in flow partitioning: at higher velocities, a
74 larger fraction of the pore volume becomes accessible to colloids, thereby decreasing their
75 exclusion from the pore space. Goppert and Goldscheider (2008) also reported that the time
76 difference between colloid and tracer breakthrough decreased with increasing velocity,
77 suggesting that higher velocities may redirect flow into smaller pores and fractures, thereby
78 enhancing colloid retention.

79 Conversely, other studies report the opposite trend, suggesting that increasing flow



80 velocity enhances hydrodynamic torque on colloids, thereby promoting detachment from
81 solid surfaces and reducing deposition. This leads to earlier breakthrough and
82 intensification of SEE. For example, Ahfir et al. (2007) observed that at higher Darcy
83 velocities (0.3483 cm s^{-1}), colloids broke through porous media earlier than conservative
84 tracers, whereas at lower velocities (0.0134 cm s^{-1}), tracers emerged first due to greater
85 colloid deposition. Similar findings were reported by Zhang et al. (2016), who noted that
86 colloids exhibited early breakthrough only when the Darcy velocity exceeded a certain
87 threshold.

88 To address these gaps in understanding SEE, this study integrates μ -CT, NMR, and
89 HYDRUS-1D modeling to clarify how flow velocity regulates SEE in porous media. μ -CT
90 and NMR were used to characterize pore-size distributions and flow heterogeneity. Column
91 experiments at different velocities, combined with HYDRUS-1D fitting, enabled the
92 quantitative determination of the size exclusion coefficient (γ). This framework establishes
93 a mechanistic link between pore structure, flow conditions, and colloid transport behavior,
94 offering a robust tool for predicting colloid fate in natural systems.

95

96 **2 Materials and Methods**

97 **2.1 Silica colloids and porous media**

98 Silica colloids were used as the model particles in this study, characterized by a
99 particle size of $0.5 \mu\text{m}$ and a zeta potential of -39.1 mV . The colloid concentration was
100 maintained at 100 mg L^{-1} . To investigate the influence of different pore structures on
101 colloid transport, high-purity quartz sands were used as the porous medium. The sands
102 were sieved into three distinct grades: fine, medium, and coarse. Before use, the quartz



103 sands were thoroughly cleaned to remove organic and iron impurities and minimize colloid
104 deposition. The sands were first soaked in a 2 mol L⁻¹ HCl solution at 90°C for 24 h (Wang
105 et al., 2025; Yan et al., 2019). After acid treatment, they were rinsed multiple times with
106 deionized (DI) water to remove residual fines and acid, followed by drying in an oven at
107 105°C (Yan et al., 2019).

108 **2.2 Column transport experiments**

109 The transport experiments were conducted in a vertical, upward-flow configuration
110 using polymethyl methacrylate (PMMA) columns (2.5 cm diameter; 10 cm or 30 cm
111 length). A peristaltic pump controlled the flow rate from the bottom of the column. The
112 sand was packed into the column under saturated conditions, supported by a nylon
113 membrane to prevent media displacement. The porosity of the packed columns was
114 approximately 0.434. To investigate the effect of flow velocity on colloid transport,
115 experiments were performed at flow rates of 10, 8, 6, 4, 2, and 1 ml min⁻¹. Before each
116 colloid transport experiment and following any change in the flow rate, a conservative
117 tracer (NaNO₃) test was performed to characterize the hydrodynamic conditions. The
118 procedure began by equilibrating the column with 5 pore volumes (PVs) of deionized (DI)
119 water. This was followed by an injection of a 0.14 PV pulse of 3 mmol L⁻¹ NaNO₃. The
120 experiment concluded with a final rinse using 5 PVs of DI water. Throughout the procedure,
121 the effluent concentration of NaNO₃ was monitored in real-time at a wavelength of 235 nm
122 using a UV spectrophotometer (TU-1900, Yoke, China).

123 The silica colloid transport experiments were similar to those used for conservative
124 tracers. After an initial flush with 5 PVs of DI water, a pulse of 0.14 PVs of the silica
125 particle suspension was introduced. This was followed by a final rinse with 5 PVs of



126 colloid-free DI water to remove unattached particles. The effluent concentrations of silica
127 colloids were quantified in real-time at a wavelength of 300 nm using the same UV
128 spectrophotometer.

129 **2.3 Pore structure characteristic**

130 The intricate pore structure of the quartz sand columns was comprehensively
131 characterized using two complementary noninvasive techniques: Nuclear magnetic
132 resonance (NMR) and X-ray micro-computed tomography (μ -CT). The experimental
133 workflow involved first performing NMR analysis on the fully saturated columns, followed
134 by oven-drying the samples for subsequent μ -CT scanning.

135 **2.3.1 NMR analysis**

136 A standard 2.0 MHz NMR analyzer (LIME-MRI-D12, Beijing Limecho Technology
137 Co., Ltd.) equipped with a 1.5-inch probe was used to determine the pore size distribution
138 (PSD) and porosity of the saturated porous media. A Carr-Purcell-Meiboom-Gill (CPMG)
139 pulse sequence was employed to measure the transverse relaxation time (T_2). The T_2
140 relaxation of water in the porous media is primarily governed by surface relaxation, which
141 is directly proportional to the pore's surface-to-volume ratio. This physical principle
142 enables a direct correlation between shorter T_2 values and smaller pores, and longer T_2
143 values with larger pores.

144 The acquired T_2 decay data are then processed to obtain a T_2 distribution spectrum.
145 This is typically done through an inverse Laplace transform algorithm, which deconvolutes
146 the multi-exponential decay signal into a continuous distribution of relaxation times. Each
147 peak in this T_2 distribution corresponds to a population of pores with a characteristic size.

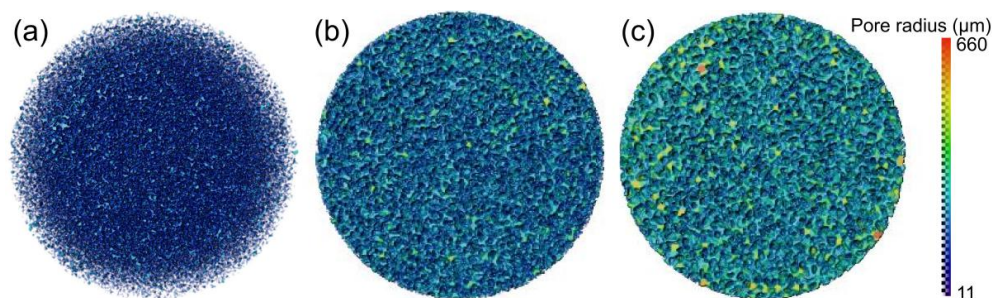


148 To convert the T_2 distribution into PSD, a conversion factor (C) is applied, based on
149 the relationship: $r = C * T_2$, where r is the pore radius. The parameter C is often determined
150 by calibrating with samples of known pore sizes or through independent measurements
151 (e.g., μ -CT).

152 2.3.2 μ -CT scanning and analysis

153 μ -CT was utilized to generate a detailed three-dimensional reconstruction of the pore
154 network. A SkyScan 1273 (Bruker, Belgium) was used to scan the samples. To balance
155 high resolution with the sample size, the 10 cm columns were scanned at a resolution of 11
156 μ m. The X-ray source was operated at 125 kV and 64 μ A.

157 The image analysis workflow was initiated by importing the raw CT slices into ImageJ.
158 The grayscale images were then converted to binary representations using an automated
159 thresholding protocol, effectively segmenting the pore space from the solid sand grains.
160 Following binarization, a noise-reduction filter was applied to remove imaging artifacts
161 before a region of interest (ROI) was cropped to focus the analysis on the central portion
162 of the sample. To further characterize the pore network, these binary slices were imported
163 into the Avizo software, which was used to generate a detailed 3D reconstruction (**Figure**
164 **1**).





166 **Figure 1.** 3D pore structure images of columns filled with three different sands. (a) fine sand, (b)
167 medium sand, and (c) coarse sand. Colors represent relative pore radii: blue corresponds to a narrow
168 pore radius, while red corresponds to a wider pore radius.
169

170 To simulate the velocity field within the pore space based on the binarized CT images,
171 a representative pore region was selected from the CT-derived longitudinal section at the
172 middle of the sand column. The selected region had a size of 300 μm in width and 100 μm
173 in height and was used to represent the local spatial distribution of pore channels and grain
174 skeletons in the porous medium. Based on the CT image segmentation results, solid grains
175 and flow-accessible pore spaces were distinguished, and the pore space was extracted as a
176 two-dimensional computational domain. A 2D finite-element model of the pore geometry
177 was developed using COMSOL (version 6.3, Burlington, MA, USA). The incompressible
178 Navier-Stokes equations were solved under steady-state conditions with a triangular mesh
179 to compute relative water velocities and streamlines surrounding the grains
180 (Sirivithayapakorn and Keller, 2003). Boundary conditions comprised no-flow walls along
181 the lateral edges orthogonal to the flow and a uniform pressure gradient between the inlet
182 and outlet.

183 **2.4. Modeling**

184 Colloid transport through saturated sand columns was simulated using HYDRUS-1D,
185 based on a one-dimensional convection–dispersion equation (CDE) considering
186 irreversible attachment and size exclusion (Bradford et al., 2003; Šimůnek et al., 2024).
187 Under steady saturated flow, the transport of a conservative tracer is described as:

$$188 \quad \frac{\partial \theta C}{\partial t} = -U \frac{\partial C}{\partial x} + \theta D_L \frac{\partial^2 C}{\partial x^2} \quad (1)$$

189 where C is the tracer concentration (mg L^{-1}), t is time (s), and x is the spatial position
190 (cm). θ is the porosity ($\text{cm}^3 \text{ cm}^{-3}$), U is the Darcy flux (cm s^{-1}), and $D_L = \alpha_L q_w$ is the



191 hydrodynamic dispersion coefficient ($\text{cm}^2 \text{s}^{-1}$). The parameter α_L was obtained by fitting
192 the tracer breakthrough curve. Assuming colloid retention does not alter porous properties,
193 colloid transport follows (Grolimund et al., 1998; Ikni et al., 2013; Kretzschmar et al.,
194 1997):

$$195 \quad \frac{\partial \theta C}{\partial t} = -q_w \frac{\partial C}{\partial x} + \theta D_L \frac{\partial^2 C}{\partial x^2} - \rho \frac{\partial S}{\partial t} \quad (2)$$

$$196 \quad \rho \frac{\partial S}{\partial t} = \theta K_r C \quad (3)$$

197 where ρ is soil bulk density (g cm^{-3}), K_r is the colloid retention rate (s^{-1}), and S is the
198 solid phase colloid concentration (mg g^{-1}). To account for size exclusion, the accessible
199 porosity for mobile colloids is expressed as (Bradford et al., 2003; Chrysikopoulos and
200 Katzourakis, 2015; Wang et al., 2024):

$$201 \quad \theta_p = \theta - \gamma \theta \quad (4)$$

202 where γ represents the fraction of pore space inaccessible to colloids (Bradford et al.,
203 2003; Wang et al., 2025; Wang et al., 2024). Substituting Eq. (4) into Eq. (2) yields:

$$204 \quad \frac{\partial \theta_p C}{\partial t} = -U \frac{\partial C}{\partial x} + \theta_p D_L \frac{\partial^2 C}{\partial x^2} - \theta_p K_r C \quad (5)$$

205 Eqs. (1)-(5) were numerically solved using HYDRUS-1D, which applies the
206 Levenberg-Marquardt algorithm to invert experimental breakthrough curves (BTCs) and
207 optimize transport parameters (Bradford et al., 2003; Šimůnek et al., 2024).

208 To compare the relative importance of advective transport and diffusion under
209 different flow velocities and column lengths, the column-scale Peclet number was
210 calculated as (Kretzschmar et al., 1997):

$$211 \quad Pe_L = \frac{vL}{D_0} \quad (6)$$



212 where v is the pore-water velocity (cm s^{-1}), calculated from the Darcy velocity U and
213 porosity θ as $v=U/\theta$; L is the column length (cm); and D_0 is the diffusion coefficient of
214 colloidal particles in water ($\text{cm}^2 \text{s}^{-1}$). For spherical colloidal particles, D_0 was estimated
215 using the Stokes–Einstein equation:

$$216 \quad D_0 = \frac{k_B T}{3\pi\mu d_p} \quad (7)$$

217 where k_B is the Boltzmann constant (J K^{-1}), T is the absolute temperature (K), μ is the
218 dynamic viscosity of water (Pa s), and d_p is the colloid particle diameter (m). The resulting
219 D_0 , originally obtained in $\text{m}^2 \text{s}^{-1}$, was then converted to $\text{cm}^2 \text{s}^{-1}$ for the calculation of the
220 Pe_L .

221

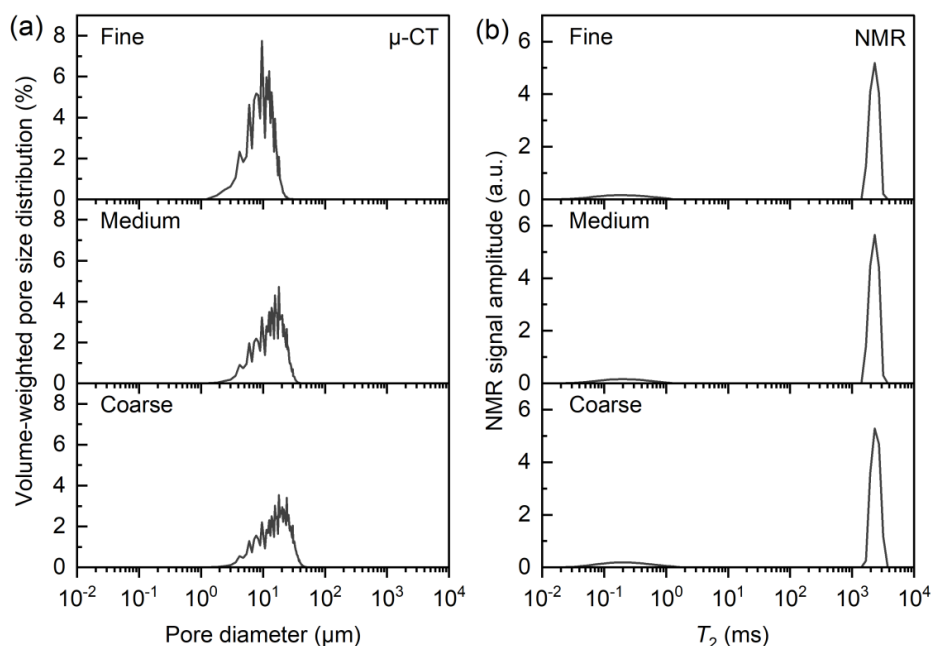
222 **3 Results**

223 **3.1 Pore size characterization**

224 **Figure 1** visualizes the reconstructed three-dimensional pore-topology structures of
225 the three sand packs from μ -CT scans. The evolution of the color gradient, from deep blue
226 to orange-red, intuitively maps the spatial distribution of pore radii: blue regions indicate
227 narrow flow pathways, whereas red regions represent more open pore spaces. From fine
228 sand (a) to coarse sand (c), the pore space undergoes pronounced geometric reorganization.
229 The fine-sand column (a) exhibits a highly compact and relatively uniform pore network,
230 with the space being almost entirely occupied by narrow flow channels (deep-blue regions).
231 Such extreme spatial confinement would substantially limit colloid transport. In contrast,
232 as the grain size increases, the coarse-sand column (c) contains markedly more large pores
233 (yellow and red patches), resulting in a much broader pore-size distribution range.



234 **Figure 2** shows the volume-weighted pore size distribution (PSD) of the sand
235 columns obtained by μ -CT and the NMR T_2 spectra distributions of the three sand types.
236 The transverse relaxation time T_2 can be converted into an equivalent pore radius, and the
237 signal amplitude is related to the pore volume of water-filled pores. Thus, the distribution
238 of NMR T_2 spectra can reflect the corresponding PSD. As shown in **Figure 2a**, one peak
239 is observed in the PSD curves obtained by μ -CT. However, as shown in **Figure 2b**, the T_2
240 spectra distributions of the column display two peaks. This discrepancy arises primarily
241 from limitations of μ -CT resolution. For instance, in the study by Peng et al. (2014), lower-
242 resolution images (e.g., 5.92 μm voxel size) fail to detect small pores below that threshold,
243 leading to underestimated porosity and surface area of Berea sandstone. Elkhoury et al.
244 (2019) highlighted that μ -CT voxel sizes of 2-10 μm underestimate porosity in sandstones
245 and limestones by missing sub-resolution pores, affecting quantitative transport
246 calculations. The small peak in the NMR spectrum located between 10^{-2} and 10^0 ms may
247 be attributed to bound water on the rough surfaces of quartz sand particles, as surface
248 roughness increases the effective surface area and enhances surface relaxation, leading to
249 faster T_2 decay and the emergence of short relaxation components (Keating, 2014).



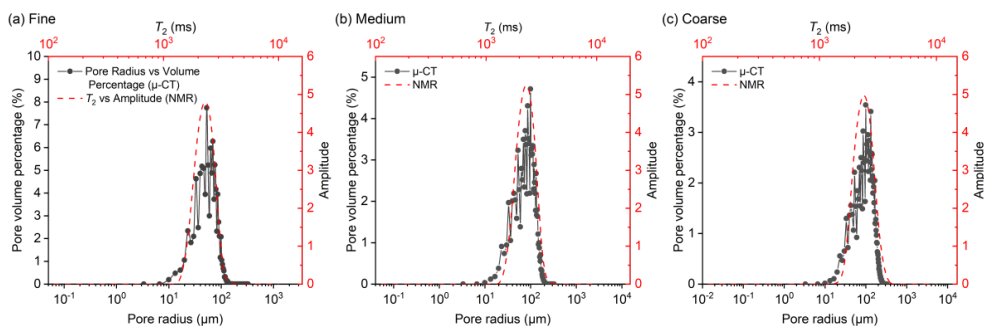
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251 **Figure 2.** Pore structure characterization of the sand columns using μ -CT and NMR. (a) Volume-
 252 weighted pore size distributions (PSD) obtained by μ -CT scanning. (b) NMR transverse relaxation time
 253 (T_2) spectra, where the signal amplitude represents the relative contribution of water-filled pores with
 254 different relaxation times. Fine sand at the top, medium sand in the middle, and coarse sand at the bottom.
 255

256 Previous studies have confirmed a correspondence between NMR- and μ -CT-derived
 257 PSD curves within intermediate pore-size ranges, often calibrated using equivalent
 258 diameter assumptions to account for geometric differences (Zhao et al., 2017). To explore
 259 this further, the radius of each pore and the corresponding pore volume obtained by μ -CT
 260 were quantified to derive the pore volume distributions of the tested cores. **Figure 3** shows
 261 the NMR T_2 spectrum curves and the pore volume distributions obtained by μ -CT for each
 262 sample. The peak of the T_2 spectrum curve aligns well with the pore volume distribution
 263 obtained by μ -CT for each sample, indicating a reliable correlation in the detectable range.
 264 However, this quantitative relationship weakens across the full T_2 spectrum, mainly



265 because X-ray scans can only detect pore sizes larger than half the voxel size (Nagel et al.,
 266 2021; Zhao et al., 2017), leading to an underrepresentation of sub-resolution pores. While
 267 the PSD measurement range of μ -CT is limited, it remains valuable for validating NMR
 268 spectra within overlapping pore-size regimes, thereby enhancing overall characterization
 269 of heterogeneous porous media, such as sand columns (Shen et al., 2025; Xiao et al., 2016;
 270 Zhao et al., 2017).



271

272 **Figure 3.** Comparison of the pore size distributions obtained using μ -CT with the distribution of
 273 transverse relaxation time T_2 obtained using NMR for the tested artificial cores. (a)-(c) show the results
 274 for the fine, medium, and coarse sands, respectively.

275

276 Combined μ -CT and NMR analyses revealed distinct pore structural characteristics
 277 among the three porous media. The PSDs of the three media types, spanning from the
 278 nanometer to micrometer scale, were derived from NMR T_2 relaxation time spectra in
 279 conjunction with μ -CT analysis (**Table 1**). The T_2 spectra were converted to PSD using a
 280 conversion factor C , calibrated to ensure consistency between the two methods within their
 281 overlapping ranges and to mitigate errors arising from microscopic heterogeneity. The
 282 conversion factor C was found to increase from the fine to the coarse media (25.0 to 42.9
 283 $\mu\text{m s}^{-1}$). This trend reflects the need to adjust the surface relaxivity coefficient as the
 284 medium coarsens. The bimodal distribution observed in the NMR T_2 spectra was



285 successfully translated into a bimodal PSD, with the two peaks corresponding to pore
286 diameters P_1 and P_2 . The diameter associated with the first peak (P_1) increased slightly
287 from $9.0 \times 10^{-3} \mu\text{m}$ for fine medium to $15.6 \times 10^{-3} \mu\text{m}$ for coarse medium. Concurrently,
288 the diameter of the second peak (P_2) exhibited a pronounced increase from 115.6 μm to
289 198.0 μm as the medium became coarser. This trend is a direct consequence of larger
290 interstitial spaces created by coarser particles (Gao et al., 2023).

291

292 **Table 1.** Pore size distribution for three media types, determined using the NMR T_2 relaxation time
293 spectra in conjunction with μ -CT analysis and a conversion factor C .
294

Media type	Total porosity (θ_{total})	C ($\mu\text{m s}^{-1}$) ^a	P_1 ($\times 10^{-3} \mu\text{m}$) ^b	P_2 (μm) ^c
Fine	0.434	25.0	9.0	115.6
Medium	0.434	39.9	14.6	184.4
Coarse	0.434	42.9	15.6	198.0

295 ^a C represents a conversion factor used to transform NMR T_2 relaxation times into pore diameters;

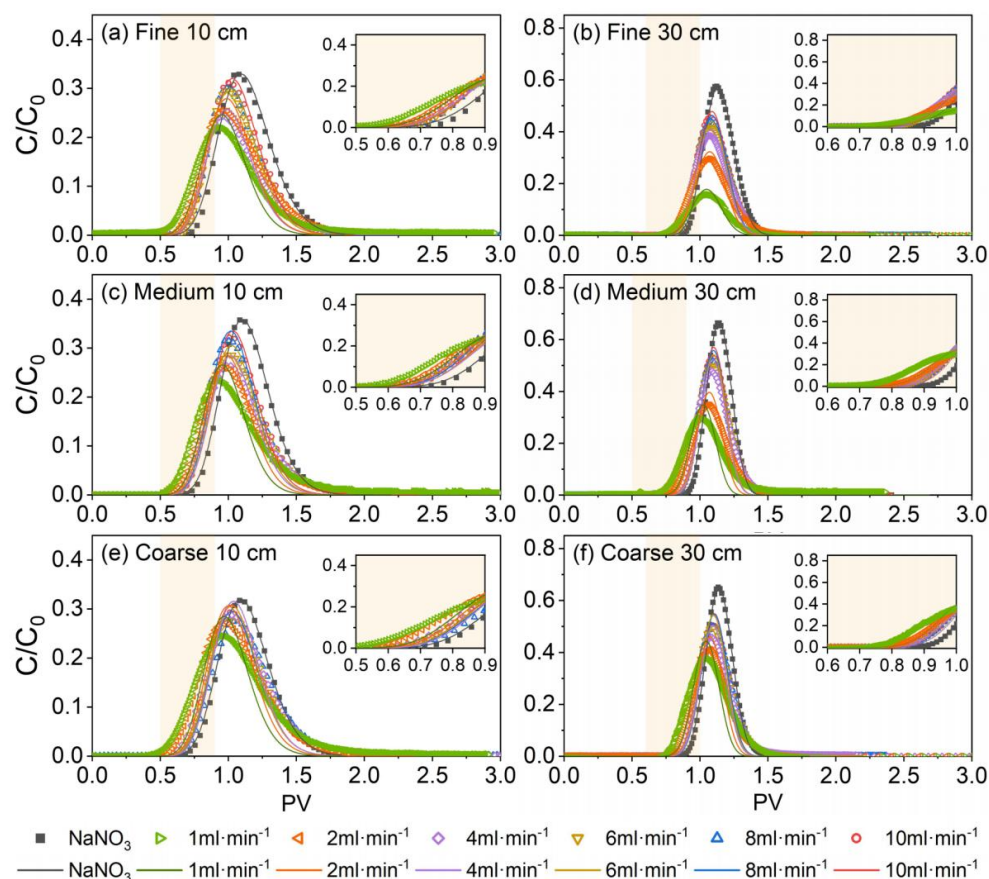
296 ^b P_1 represents the pore diameter corresponding to the first peak in the NMR PSD;

297 ^c P_2 represents the pore diameter for the second peak in the NMR PSD.

298

299 3.2 Colloid breakthrough curves

300 **Figure 4** presents the observed and fitted breakthrough curves (BTCs) of a
301 conservative tracer (NaNO_3) and 0.5 μm silica colloids in sand columns. The columns, 10
302 cm and 30 cm long, were packed with fine, medium, and coarse quartz sands. The results
303 demonstrate that the peak and shape of the BTCs are strongly dependent on flow velocity.
304 Crucially, the colloids consistently exhibited an earlier breakthrough compared to the
305 conservative tracer. This phenomenon provides compelling evidence of the size exclusion
306 effect (SEE), highlighting the distinct transport kinetics of colloids relative to the solute
307 transport signals.



308

309 **Figure 4.** The observed and fitted breakthrough curves of NaNO_3 and silica colloids in saturated porous
 310 media at different flow rates: in fine sand with column lengths of 10 cm (a) and 30 cm (b), medium sand
 311 with column lengths of 10 cm (c) and 30 cm (d), and coarse sand with column lengths of 10 cm (e)
 312 and 30 cm (f). A small inset image in the upper right corner of each figure displays a magnified view of the
 313 highlighted yellow region.

314

315 Additionally, the BTCs of the colloids exhibit a strong dependence on the flow rate.
 316 As the flow velocity increases, the BTC peaks for silica colloids become notably sharper,
 317 accompanied by a marked increase in the overall recovery rate (**Table 2**). At lower flow
 318 rates ($1\text{--}4\text{ ml min}^{-1}$), the peak effluent concentrations were low with recoveries ranging
 319 from 0.5 to 0.9. In contrast, higher flow rates ($6\text{--}10\text{ ml min}^{-1}$) yield elevated recovery,



320 reaching approximately 0.7-1.0. This phenomenon reflects the dual role of flow rate in
321 regulating colloid deposition kinetics. First, higher flow velocities significantly shorten the
322 residence time of colloids within the porous media, reducing the probability of particles
323 contacting and attaching to solid surfaces. Second, increased flow rates strengthen local
324 hydrodynamic shear, which effectively weakens the interaction between colloids and media
325 surfaces, thereby suppressing the tendency for deposition. These results align with
326 established transport principles, where higher velocities typically reduce particle retention
327 and enhance mobility (Ahfir et al., 2007; Benamar et al., 2005). Similarly, Kretzschmar
328 and Sticher (1998) observed stronger breakthrough for latex microspheres at higher flow
329 rates. Torkzaban et al. (2015) further demonstrated that increased shear associated with
330 higher velocities weakens colloid-surface interactions, thereby reducing deposition and
331 promoting particle mobility.

332

333 **Table 2.** Experimental and fitted parameters for colloid transport in three types of porous media under
334 different Darcy velocities.



Media type	Column length (cm)	Flow velocity (ml min ⁻¹)	Darcy velocity (cm s ⁻¹)	Dispersion (cm)	Effective porosity (cm ³ cm ⁻³)	γ (-)	Recovery rate (-)
Coarse	30	10.091	0.032	0.091	0.425	0.020	0.937
	30	8.306	0.026	0.091	0.419	0.034	0.946
	30	6.179	0.019	0.091	0.420	0.033	0.942
	30	4.104	0.013	0.091	0.418	0.038	0.906
	30	2.142	0.007	0.091	0.410	0.054	0.790
	30	1.126	0.004	0.091	0.405	0.066	0.728
	10	9.376	0.029	0.147	0.409	0.058	0.990
	10	7.773	0.024	0.147	0.408	0.060	0.956
	10	6.001	0.019	0.147	0.407	0.062	0.946
	10	4.209	0.013	0.147	0.405	0.066	0.914
	10	2.184	0.007	0.147	0.400	0.079	0.828
	10	1.181	0.004	0.147	0.384	0.116	0.826
	30	9.813	0.031	0.080	0.417	0.039	0.929
	30	8.064	0.025	0.080	0.418	0.037	0.888
Medium	30	6.299	0.020	0.080	0.416	0.041	0.823
	30	4.219	0.013	0.080	0.416	0.042	0.832
	30	2.255	0.007	0.080	0.411	0.054	0.627
	30	1.177	0.004	0.080	0.401	0.077	0.645
	10	9.963	0.031	0.135	0.407	0.062	0.955
	10	8.172	0.026	0.135	0.408	0.061	0.944
	10	5.901	0.019	0.135	0.407	0.062	0.909
	10	3.944	0.012	0.135	0.407	0.063	0.892
	10	2.083	0.007	0.135	0.399	0.081	0.804
	10	1.156	0.004	0.135	0.383	0.118	0.741
	30	10.108	0.032	0.127	0.417	0.038	0.877
	30	8.011	0.025	0.127	0.418	0.038	0.806
	30	6.009	0.019	0.127	0.418	0.036	0.737
	30	4.291	0.013	0.127	0.414	0.046	0.547
Fine	30	2.333	0.007	0.127	0.408	0.060	0.547
	30	1.202	0.004	0.127	0.401	0.076	0.549
	10	10.005	0.031	0.156	0.408	0.061	0.947
	10	7.848	0.025	0.156	0.406	0.065	0.927
	10	5.915	0.019	0.156	0.408	0.061	0.902
	10	3.918	0.012	0.156	0.394	0.092	0.820
	10	2.162	0.007	0.156	0.392	0.098	0.814
	10	1.175	0.004	0.156	0.373	0.141	0.700

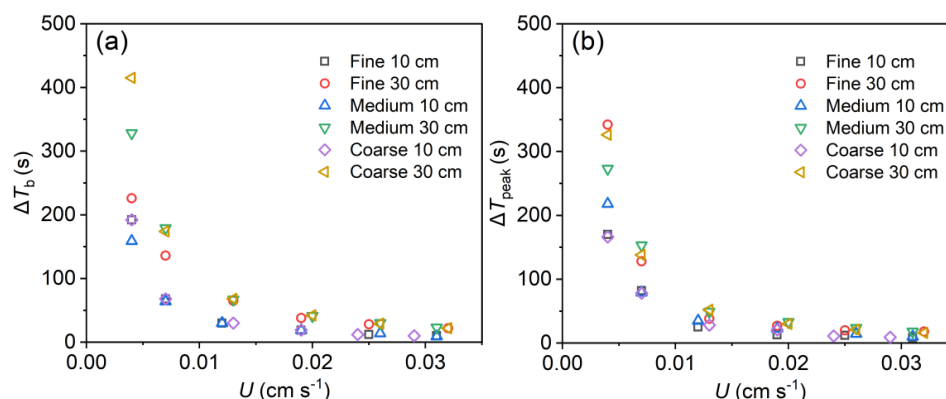
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336 To further analyze the size exclusion behavior, the relationships between flow velocity

337 and two characteristic parameters of early breakthrough were examined (Figure 5). These



338 parameters were ΔT_b (the relative time difference at $C/C_0=0.05$) and ΔT_{peak} (the relative
 339 time difference at the peak concentration) between colloids of different sizes and a
 340 conservative tracer. Larger ΔT values (for both ΔT_b and ΔT_{peak}) indicate more pronounced
 341 early breakthrough and a size exclusion effect. The results consistently showed that as flow
 342 velocity (U) increased, both ΔT_b and ΔT_{peak} decreased significantly, for all three media and
 343 both column lengths.



344

345 **Figure 5.** The relationship between the difference in breakthrough times (ΔT_b , a) and peak arrival times
 346 (ΔT_{peak} , b) between colloids and a conservative tracer as a function of Darcy velocity (U) in different
 347 sand (fine, medium, and coarse) columns of different lengths (10 and 30 cm).

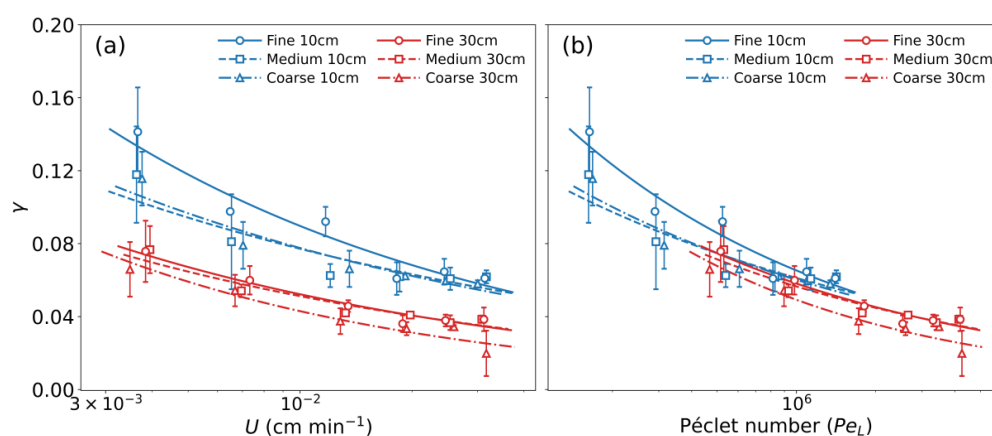
348

349 3.3 The size exclusion parameter γ

350 Given that analyzing the SEE of colloids based on ΔT values provides a relatively
 351 macroscopic perspective, Hydrus-1D modeling was employed to quantify SEE using the
 352 fitted parameter γ (Bradford et al., 2003; Wang et al., 2025; Wang et al., 2024). In this
 353 numerical framework, γ represents the fraction of water saturation that is inaccessible to
 354 mobile colloids. The fitted results are presented in **Table 1**, and the relationship between
 355 Darcy velocity and γ is shown in **Figure 6**. It is evident that γ exhibits an inverse



356 relationship with flow velocity across all media types and column lengths. The reduction
 357 in γ is most pronounced in the low-velocity regime. In particular, for $U < 0.01 \text{ cm s}^{-1}$, γ
 358 exhibits a sharp decline, whereas the rate of decrease becomes progressively smaller at
 359 higher velocities, indicating a clear nonlinear sensitivity to flow conditions. For instance,
 360 in the 30 cm coarse sand column, γ is only 0.032 at a velocity of 0.032 cm s^{-1} , but it rises
 361 to 0.087 when the velocity drops to 0.004 cm s^{-1} . This dynamic behavior of γ is consistent
 362 with the previously observed inverse relationship, in which ΔT decreases as flow velocity
 363 increases.
 364



365
 366 **Figure 6.** Variation of size exclusion parameter γ with hydrodynamic conditions. (a) the relationship
 367 between γ and Darcy velocity (U); (b) the relationship between γ and Péclet number (Pe). Dashed lines
 368 represent fitted power-law regressions.

369
 370 To further evaluate the role of hydrodynamic conditions, γ was also plotted against
 371 the Péclet number (Pe) in **Figure 6b**. The same monotonic decrease was observed, showing
 372 that the weakening of SEE is associated not only with increasing Darcy velocity, but also
 373 with the increasing dominance of advective transport relative to diffusive exchange. This



374 result suggests that γ is not merely a geometric descriptor of pore space, but a dynamic
 375 parameter that is strongly modulated by hydrodynamic conditions.

376 The dashed lines in **Figure 6** represent power-law regressions fitted to the γ - U and γ -
 377 Pe relationships, and the corresponding parameters are summarized in **Table 3**. Overall,
 378 the regressions provided good fits to the experimental data ($R^2 = 0.883$ – 0.997 for γ - U and
 379 $R^2 = 0.926$ – 0.987 for γ - Pe). Although the fitted coefficient a varied among media and
 380 column lengths, the exponent b was consistently negative, confirming the inverse
 381 dependence of γ on hydrodynamic forcing. Moreover, the absolute value of b tended to be
 382 larger in the coarse sand, particularly for the 30 cm column, implying a stronger sensitivity
 383 of γ to flow conditions in more open pore networks.

384

385 **Table 3.** Parameters fitted to the functional relationships between γ and U or Pe .

Media type	Column length (cm)	a ($s^b \text{ cm}^{-b}$)	b (-)	R^2	Equation
Fine	10	0.017	-0.374	0.964	$\gamma = a \cdot U^b$
Fine	30	0.010	-0.383	0.926	
Medium	10	0.016	-0.392	0.963	
Medium	30	0.007	-0.454	0.949	
Coarse	10	0.015	-0.384	0.967	
Coarse	30	0.005	-0.526	0.987	
Fine	10	15.235	-0.395	0.919	$\gamma = a \cdot Pe^b$
Fine	30	8.707	-0.363	0.927	
Medium	10	3.306	-0.289	0.823	
Medium	30	5.901	-0.336	0.916	
Coarse	10	4.769	-0.317	0.929	
Coarse	30	28.638	-0.461	0.870	

386

387 **4 Discussions**



388 The apparent dependence of γ on flow velocity, as observed in Table 2 and Figure 6.
389 By definition, γ represents the accessible pore fraction for mobile colloids and, from a
390 purely geometric perspective, should primarily be governed by the size ratio between
391 colloids and pore structures. However, in practice, finite-sized particles do not uniformly
392 sample the entire pore space but instead interact selectively with the pore-scale velocity
393 field. As demonstrated by James and Chrysikopoulos (2003), finite-size colloids are
394 excluded from near-wall low-velocity regions and preferentially travel along faster
395 streamlines, resulting in effective velocities exceeding the mean fluid velocity.
396 Consequently, γ inferred from BTC fitting reflects an effective transport parameter rather
397 than a fixed geometric fraction independent of flow.

398 The inverse relationship between γ and flow velocity observed in this study is
399 consistent with previous studies reporting that colloid early breakthrough becomes less
400 pronounced as velocity increases. Massei et al. (2002) found that the temporal separation
401 between colloid and solute breakthrough decreased with increasing Darcy velocity, while
402 Bai et al. (2015) similarly reported weaker preferential colloid breakthrough at higher
403 seepage velocities. Goppert and Goldscheider (2008) also showed that the difference
404 between colloid and solute transport diminished under high-flow conditions. These studies
405 collectively support the idea that increasing flow velocity expands the effective flow
406 domain involved in colloid transport, thereby reducing the apparent excluded fraction.

407 At low flow velocities, the pore-scale velocity field is more strongly partitioned into
408 high-velocity channels and weakly advective or quasi-stagnant regions. Under such
409 conditions, colloids remain concentrated in a limited number of preferential pathways,
410 whereas adjacent low-velocity pore domains are only weakly sampled within the



411 experimental timescale. Pore-scale simulations by Samari Kermani et al. (2020)
412 demonstrated that low-flow conditions favor particle retention and nonuniform transport
413 in constricted and poorly connected pores. Mao et al. (2020) further reported that low
414 velocity enhances localized retention in heterogeneous porous media. In addition, Zhao et
415 al. (2020) showed that lower velocities can prolong colloid residence near collector
416 surfaces, thereby increasing the likelihood of deposition under favorable interfacial
417 conditions.

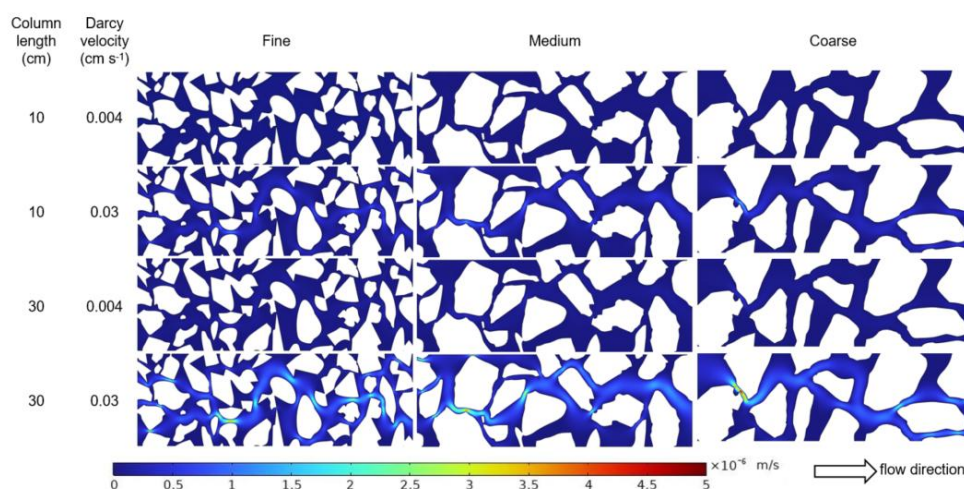
418 As flow velocity increases, the pore-scale flow field undergoes systematic
419 reorganization. Enhanced hydraulic gradients at pore throats increase hydrodynamic drag
420 forces, reducing colloid residence in low-velocity zones (Nishad et al., 2021). At the same
421 time, colloid sampling of the velocity field shifts toward sustained transport along
422 connected high-velocity pathways, decreasing the likelihood of entering or remaining in
423 stagnant zones. Pore-scale modeling confirms that increased flow velocity enhances the
424 continuity of active flow paths and reduces localized retention (Samari Kermani et al.,
425 2020). Consequently, flow pathways that are effectively inaccessible under low-flow
426 conditions become increasingly utilized at higher velocities, leading to an increase in
427 effective pore accessibility and a corresponding decrease in γ .

428 These analyses were further supported by finite element flow simulations (**Figure 7**).
429 At low velocity (0.004 cm s^{-1}), the simulated velocity field exhibited extensive dark-blue
430 zones near pore walls and throats, indicating slow-flow regions. With higher velocity (0.03
431 cm s^{-1}), the flow field transitioned to light-blue and yellow regions, indicating the activation
432 of smaller pores and the formation of more continuous flow pathways. It should be
433 emphasized, however, that the μ -CT resolution of $11 \text{ }\mu\text{m}$ does not allow direct resolution



434 of the sub-micron pores inferred from the NMR T_2 spectra. Thus, the simulations should
435 not be interpreted as direct evidence that colloids entered unresolved micropores at higher
436 velocity. Rather, they provide indirect support for a redistribution of the pore-scale
437 hydraulic field.

438



439

440 **Figure 7.** Finite element flow simulations for different column lengths (top to bottom), quartz sand
441 media types (left to right), and Darcy velocities.

442

443 5 Conclusions

444 By integrating NMR, μ -CT, column experiments, and HYDRUS-1D modeling, this
445 study systematically quantified the influence of flow velocity on the size exclusion
446 transport of colloids in saturated porous media. Colloids consistently broke through earlier
447 than the conservative tracer, confirming the occurrence of size exclusion across all tested
448 media. However, the strength of this effect decreased with increasing flow velocity, as
449 demonstrated by both the breakthrough-time metrics and the fitted size exclusion



450 coefficient γ . These results indicate that colloid exclusion is governed not only by pore-
451 size constraints, but also by hydrodynamic regulation of pore-space accessibility.

452 The fitted γ values showed that γ is best understood as a flow-dependent effective
453 parameter rather than a fixed geometric property. Under low-flow conditions, colloid
454 transport was concentrated in preferential pathways, leading to a larger apparent
455 inaccessible pore fraction; under higher velocities, more of the pore network became
456 hydraulically accessible, resulting in smaller γ values. Column length further modulated
457 this behavior, with shorter columns generally exhibiting stronger apparent exclusion than
458 longer columns. Together, these findings demonstrate that colloid size exclusion reflects
459 the coupled effects of pore structure, flow conditions, and transport distance, and they
460 provide a stronger physical basis for predicting colloid transport in natural and engineered
461 subsurface systems.

462



463 **Authorship contribution**

464 **Changxi Wang:** Data curation, Investigation, Methodology, Formal analysis,

465 Visualization, Writing – original draft.

466 **Zhaofei Duan:** Investigation, Methodology.

467 **Xinlin Li:** Investigation.

468 **Ziyu Zhou:** Investigation, Data curation.

469 **Jirka Šimůnek:** Supervision, Writing – review & editing.

470 **Renkuan Liao:** Conceptualization, Supervision, Resources, Funding acquisition,

471 Writing – review & editing

472 **Conflict of Interest**

473 The authors declare no conflicts of interest relevant to this study.

474 **Data Availability Statement**

475 All data supporting the findings of this study are openly available. The NMR

476 measurements, μ -CT pore-structure data, colloid breakthrough curves, and size exclusion

477 parameters are available at Wang (2025).

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481



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