The influence of various solvents extraction on chemical properties on Chang 7 shale, Ordos Basin, China

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Abstract. To explore the effect of various solvents extraction on the chemical property of shales, several lacustrine shales from Chang 7 member of the Upper Triassic Yanchang Formation, Ordos Basin with maturities from marginally mature (T_{max}=439°C) to late mature (T_{max}=456°C) were extracted by using acetone, tetrahydrofuran (THF), carbon disulfide (CS₂), and benzene, respectively. Fourier transform infrared spectroscopy (FTIR) was employed to examine the functional groups of the samples before and after extraction with different solvents. The results showed that the extraction yield from shale with THF is significantly higher than that of other solvents, which may be related to the properties of the THF, including the aromatic structure, high boiling point, excellent Hansen solubility parameters, and strong polarity. The total organic carbon (TOC)-normalized yield of the mature sample J1 is significantly higher than that of other samples, which may be related to that the J1 sample is at the peak of hydrocarbon generation, thus a large number of kerogens were cracked into oil and bitumen. The aromaticity of organic matter (OM) increases with the increase of maturity. The length of the aliphatic chains of the OM first increased with the increase of maturity before late maturity stage, and then decreased in late maturity stage. The extraction of shales with solvents hardly changes the length of aliphatic chains. Higher aromaticity is observed in shale residues after THF extractions than other solvents (i.e., acetone, CS₂, benzene).

1 Introduction

Due to the increasingly serious energy shortage problems associated with the exhaustion of fuel energy resources, potential unconventional fossil sources are highly desired (Yang et al., 2019; Li et al., 2022). The quest to product unconventional petroleum-based fuels and achieve energy independence is being aggressively pursued in China and the United States (Overland, 2015). In the past few years, shale oil has been regarded as an important resource that can be exploited commercially due to the technical innovations of three-dimensional development in horizontal wells and fracture-controlled fracturing (Li et al., 2019; Zhou et al., 2020a; Lei et al., 2021; Yang et al., 2021a). For China, the government has been encouraging shale oil developments to address the shortage of domestic oil resources, and the rising energy demand and to safeguard the country's long-term energy security (Yang et al., 2019; Hu et al., 2020; Zhou et al., 2020b; Lu et al., 2022).

Extraction has become a common shale pretreatment method in the laboratory to study the pore structures related to OM (Qi et al., 2019; Wang et al., 2020; Yang et al., 2021b). However, different solvents could affect shale extraction efficiency and methane adsorption capacity (Cao et al., 2019, 2020). For the shale samples, the extraction by using acetone, CS₂, and benzene can be used to reveal the micropores, mesopores, and macropores, respectively (Cao et al., 2019). In addition, during the development of shale oil, the chemical properties of shale after being extracted by using different organic solvents are also different (Cao et al., 2020). Wei et al. (2014) found that the hydrocarbons in toluene extract exhibit remarkable aromaticity. Furmann et al. (2013) showed that the organic aromaticity of extractions from dichloromethane is greater than that from methanol.

A large number of studies focus on either the changes in shale pore structure before and after extraction (Gorynski et al., 2019; Qi et al., 2019; Yang et al., 2021a,b) or the functional groups of OM extracted from underground fossil energy (Chen et al., 2012; Mastalerz et al., 2012; Furmann et al., 2013; Wei et al., 2014). In fact, underground shale is often washed out of OM by organic solvent extraction in the laboratory to explore the relationship between OM and inorganic mineral skeleton in shale. It is worth mentioning that this study is a continuation of our earlier published study, which details the findings about influence of extraction on shale pore structure with different maturity using various solvents (Cao et al., 2019, 2020). However, the study of the changes in chemical properties in lacustrine organic-rich shale of different maturity before and after extraction with different solvents is rarely reported. Our results of the study will help in the selection of organic solvents for oil-washing experiments in shales of different maturity.

Fourier Transform Infrared Spectroscopy (FTIR) is an advanced method for the determination of chemical structures (e.g., functional groups) of OM (Wei et al., 2014). In this study, several lacustrine shales with different maturities from Chang 7 member of the Upper Triassic Yanchang Formation, Ordos Basin, central China were collected. The present study is a continuation of our previous research (Cao et al., 2019, 2020), soxhlet extractions with four different solvents (tetrahydrofuran, carbon disulfide, benzene, and acetone) were performed on the selected shale samples. Interestingly, the Fourier Transform Infrared Spectroscopy (FTIR) was performed on the samples before and after the extraction. After that, the influence of various solvent extraction on chemical properties in lacustrine shale of different maturity was summarized.

1 Geological settings and samples

According to the basement and faults, the Ordos Basin is divided into six secondary structural units, namely the Weibei uplift, the Yishan slope, the Tianhuan depression, the Yimeng uplift, the western margin thrust belt, and Jinxi flexural fold belt (Fig. 1) (Guo et al., 2014). The Yishan slope is inclined to the west with a slope of about 1° (Guo et al., 2014). The Chang 7 member was developed during the largest lacustrine flooding in the lake basin (Fig. 1) (Guo et al., 2014). Yellowish tuff intervals are interbedded within the Yanchang sediments ranging from 0.2 to 0.45 cm (0.08–0.18 in.) (Qiu et al., 2014).

The Yanchang Formation of the upper Triassic can be divided into 10 sub-segments (i.e., Chang 1-10) (Fig. 2). The Chang 7 member is mainly made up of silty mudstone and shales and has great potential for shale oil/gas (Fig. 2) (Duan et al., 2008;

Lei et al., 2015). The Chang 7 member shale develops a large area of high-quality source rocks (about 5×10^4 km²), which is rich in oil-prone OM derived from acritarchs (Leiosphaeridia species) as well as some Botryococcus (Ji et al., 2010). The cumulative thickness is mostly between 10 m and 50 m, and the maximum thickness can reach more than 80 m (Guo et al., 2014). In this paper, several shale samples with different maturities in Chang 7 member of the Upper Triassic Yanchang Formation were obtained from wells Huan 317, Jian 1, Luohe 10, and Jinghe 2, respectively (Fig. 1). The samples selected for this study have been analyzed in our previous publications (Cao et al., 2020).

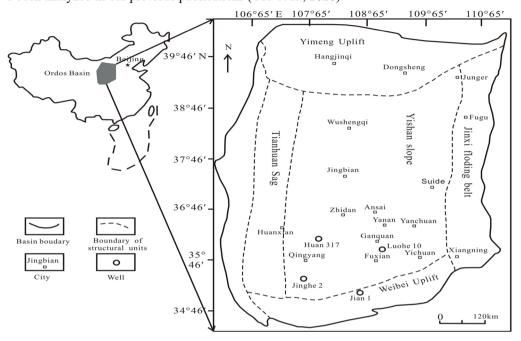


Fig. 1. Locations of sampling wells and simplified structural framework across the Ordos Basin (modified from Cao et al. 2019).

Epoch	Formation	Subsection	Lithology	Sedimentary	Thinkness
Lower	Tormation	Yan-1to	column	facies	(m)
Jurassic	Yanan	Yan-10	=	Fluvial- Lacustine-	250-300
		Chang1	0 0 0 0 0	Svamp	0-245
		Chang2			120-160
		Chang3	<u></u>		100-170
		Chang4+5		Fluvial- lacustrine	90-130
	Yanchang	Chang6	= = = = = = = = = = = = = = = = = = =		180-200
Upper Triassic		Chang7		Deep- lacustrine	
		Chang8		Lacustrine	100-190
		Chang9			
		Chang10		Fluvial	200-320
000	Conglomerate	· · · · · ·	Sandstone	Sandy	mudstone
	Mudstone	$\begin{array}{c c} A & A & A \\ \hline A & A & A \end{array}$	Dil shale	Coal	

Fig. 2. The strata and sedimentary characteristics of the Yanchang Formation of the Upper Triassic (modified from Cao et al. 2020).

3 Experiments

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3.1 Geochemical analysis

The samples were crushed to 180-200 mesh prior to geochemical analysis. The TOC content was tested by a Leco C/S-344 Carbon/Sulfur analyzer. The type, maturity, and hydrocarbon generation potential of OM were determined. The temperature at which the most S₂ is generated is regarded as the maximum pyrolysis yield temperature (T_{max}, °C) and the hydrogen index (HI, mg HC/g TOC) was obtained from the ratio of S₂ to TOC (Peters, 1986).

3.2 X-ray diffraction

The samples were tested by a D/max-2500 diffractometer, and the tests follow two separate processes of the CPSC procedure (China Petroleum Standardization Committee, 2010). The actual mineral content of the samples was obtained by quantitative X-ray diffraction (XRD) analysis of samples smaller than 200 mesh (<0.075 mm).

3.3 Soxhlet extraction

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The bulk shale samples were uniformly crushed into 60 mesh with a laboratory knife mill and then evenly divided into five parts. The sample was extracted using solvents of different aromaticity, polarity, and permeability, namely acetone, tetrahydrofuran, carbon disulfide, and benzene, and the remaining original sample was used as a control. About 1000g solvent and 50g shale sample were sealed in a Soxhlet extractor to prevent solvent loss. The extraction time lasted 150h until the solvent is colourless. Samples were named according to their corresponding abbreviated well names (JH2, J1, LH10, and H317) (Table 2), and the original shale samples were marked by the shorthand subscript following the sample name (JH2_{orig}, J1_{orig}, LH10_{orig}, and H317_{orig}). The residue (e.g., JH2) from THF, acetone, CS₂, and benzene extraction was clearly characterized by JH2_T, JH2_A, JH2_C, and JH2_B, respectively.

3.4 Potassium bromide (KBr)-FTIR analysis

Both powdered original shale samples and their corresponding extracted shale residues (~2mg) were blended with potassium bromide (KBr, ~200mg) and pressed into pellets. Through the use of a Nicolet 6700 FT-IR spectrometer collecting 200 scans per sample at a resolution of 4 cm⁻¹, the vibration frequencies of specific atomic bonds were analyzed. Thus, the chemical functional groups could be assessed using a standard semi-quantitative technique. For KBr-FTIR characterization, each spectrum was recorded in the spectral range of 400-3250 cm⁻¹. The bands of absorption were identified by comparing the spectrums with published studies (Drobniak and Mastalerz, 2006; Furmann et al., 2013).

According to a manual mode, the band area was determined using the ORIGIN software. These integrated band areas were used to calculate ratios for (1) aromaticity: $AR1=[(\delta Ar C = C/v Al C-H) + \delta Ar C=C]$, AR2=(v Ar C-H/v Al C-H), $AR3=(\gamma Ar C-H/v Al C-H)$; (2) length of aliphatic chains: $LAC=(CH_2/CH_3)$ in v Al C-H and (3) degree of substitution (DOS) of aromatic sites by alkyl groups: $DOS=(\gamma Ar C-H)$ (1 adjacent H)/ γ Ar C-H (4 adjacent H)) (Wei et al., 2014). The detailed definitions of the parameters can be found in Tables 1 and 4.

The representative spectrums of the original shales and corresponding residues are presented in Fig. 5 and Fig. 6, respectively. In terms of the length of aliphatic chains (LAC), longer n-alkyl chains are determined by CH₂ bands, whereas shorter n-alkyl and branched aliphatic chains are indicated by CH₃ bands (Table 4). The DOS of aromatic rings represents the fraction of aromatic sites where hydrogen atoms are substituted by alkyl groups (Table 4).

Table 1. Fourier Transform Infrared (FTIR) bands used in this study (Chen et al., 2012).

FTIR band	For marginally mature shales	For mature shales	For late mature shale	For late mature shale	
r i ik band	JH2 T _{max} (439°C)	J1 T _{max} (449°C)	LH10 T _{max} (454°C)	H317 T _{max} (456°C)	
•	Wave numbers (cm ⁻¹)				
ν Ar C-H	3046-2992	3062-2992	3084-3005	3062-3000	
ν Al C-H	2970-2812	2970-2809	2983-2809	2984-2814	
$\nu_{as} \; CH_3$	2970-2874	2970-2877	2970-2887	2984-2882	
$\nu_s \ CH_2$	2874-2812	2877-2809	2887-2798	2882-2814	
δ Ar C=C	1705-1575	1701-1561	1719-1552	1707-1552	
δ Al C-H	1484-1386	1477-1400	1487-1389	1482-1381	
γ Ar C-H	945-667	946-673	939-673	948-673	
γ Ar C-H 1	945-833	930-886	940-812	948-817	
γ Ar C-H 2	833-721	814-707	812-709	817-707	
γ Ar C-H 4	721-667	707-673	709-673	707-673	

Ar–aromatic; Al–aliphatic; v–stretching vibration; δ –deformation vibration in plane; γ –deformation vibration out of plane; as–asymmetric; s–symmetric.

4 Results

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115 4.1 Geochemical characteristics

The geochemical features of shales were listed in Table 2. Four selected samples span from marginally mature (JH2, 439°C) to Late mature (H317, 460°C) based on the Chinese continental hydrocarbon source rock geochemical evaluation method (SY/T 5735-1995). The kerogen type of selected samples is type I or II₁ (Fig. 3) (Tong et al., 2011). TOC content is generally high, ranging from 3.79 to 22.19 wt.% (Table 2). The hydrocarbon generation potential (S_1+S_2) ranges from 8.11 mg/g to 127.42 mg/g. Table 2 shows that the hydrogen index (HI) of the samples is in the range of 155 mg/g~528 mg/g.

Table 2. Geochemical features of the original shale samples and the corresponding residues.

Sample	$S_1(mg/g)$	$S_2(mg/g)$	$T_{max}(^{\circ}C)$	TOC (%)	OM type	HI (mg/g)	Maturity stage
JH2	10.19	117.23	439	22.19	I	528	Marginally mature
J1	2.23	5.88	449	3.79	II_1	155	Mature
LH10	11.31	47.42	454	16.23	I	292	Late mature
H317	5.39	33.89	456	18.03	I	188	Late mature

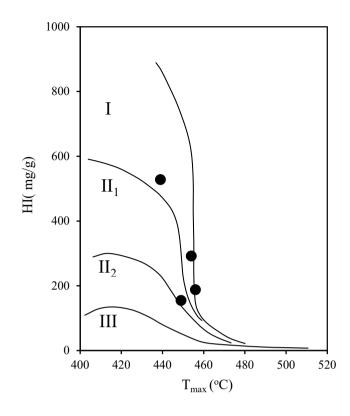


Fig. 3. Plot of HI versus T_{max} for the original shales (based on Espitalie et al. 1985)

4.2 Mineral compositions

The samples contain a large amount of clay minerals (42.8 wt. %-54.2 wt. % with an average of 48.15%). Illite/smectite mixed-layer or Illite are the most dominant clay types (Table 3). In general, the content of the felsic component is between 19.5 wt. %-52.2 wt. % with the average of 40.63%. In addition, the pyrite content of the studied samples varies greatly, ranging from 0.9 to 25.5 wt.% (Table 3).

Table 3. Mineral compositions of the studied samples.

Sample	Quartz (wt. %)	Feldspar (wt. %)	Pyrite (wt. %)	Gypsum (wt. %)	All clays (wt. %)	Illite/Smectite (wt. %)	Illite (wt. %)	Kaolinite (wt. %)	Chlorite (wt. %)	Mixed-layer ratio (I/S) S, %
JH2	12	7.5	25.5	0.8	54.2	70	9	21	/	19
J1	36.5	12.7	0.9	/	49.9	62	18	8	12	18
LH10	23.2	29	2.1	/	45.7	66	15	7	12	11
H317	29.7	11.9	15.6	/	42.8	2	88	2	8	24

^{/,} the content of individual mineral was not determined.

130 4.3 Extraction yields

The extraction data of the studied samples with different solvents is shown in Fig. 4. Among all the solvents, THF has the highest extraction efficiency (2.44 wt. %-4.43 wt. %) (Fig. 4a). According to the TOC-normalized yield of extracts, the mature samples J1 (T_{max} 449°C) had significantly higher extractable (13.48 wt. %-56.91 wt. %) than other samples (\leq 5.28 wt. %) (Fig. 4b).

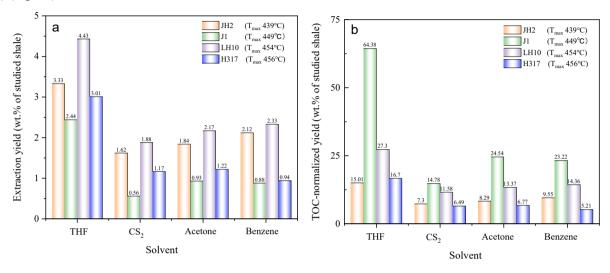


Fig. 4. Extraction data of the studied samples with solvents of acetone, THF, benzene, and CS₂ (a. original extraction yield b. TOC-normalized yield of extracts).

4.4 FTIR spectroscopy

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The representative spectrums of the original shales and corresponding residues are presented in Fig. 5 and Fig. 6, respectively. The FTIR results after extraction are summarized in Table 4. The OM in shale is a three-dimensional macromolecule composed of aromatic clusters and aliphatic chains (Tong et al., 2011; Guan et al., 2015; Wang et al., 2016; Wang et al., 2017; Zhao et al., 2018). The aromaticity (i.e., AR2 and AR3) of the samples follows the order: H317 (3.327) > LH10 (3.225) > J1 (3.038) > JH2 (2.828) (Table 4), which are consistent with maturity. In addition, shale residues from THF extraction possess higher aromaticity than those from other solvents. Unlike aromaticity, the length of aliphatic chains (LAC) doesn't increase monotonically with the increase of maturity (Table 4). However, there is no regularity in the DOS (i.e., the fraction of aromatic sites where hydrogen atoms are substituted by alkyl groups) of different maturity shales, and the DOS of shale before and after extraction with different solvents demonstrated an irregular change (Table 4).

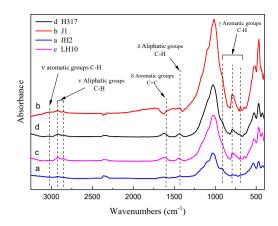


Fig. 5. FTIR spectra of original (a) marginally mature sample $JH2_{orig}$ (T_{max} =439°C) (b) the mature sample $J1_{orig}$ (T_{max} =449°C) (c) late mature sample $LH10_{orig}$ (T_{max} =454°C) and (d) late mature sample $H317_{orig}$ (T_{max} =456°C).

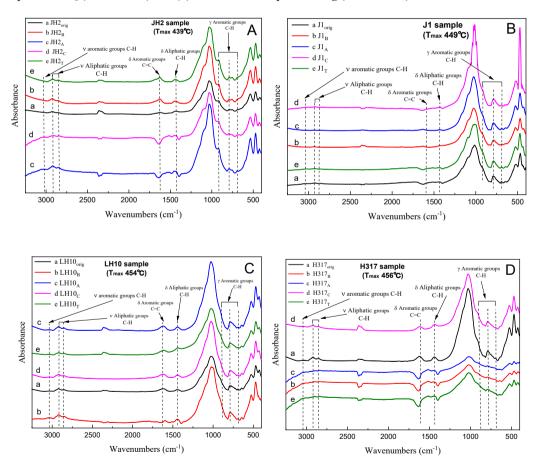


Fig. 6. A comparison of FTIR spectra of original samples and residues.

Table 4. FTIR results from original shales and extracted shale residues.

	FTIR absorbance ratios*					
	AR1 [#]	AR2	AR3	LAC	DOS	
Shale residues after extraction:						
JH2 shale:						
Original shale	2.352	0.010	2.818	0.242	11.498	
After extraction with:						
acetone	0.000	0.039	2.156	0.288	8.935	
CS_2	0.000	0.092	2.449	0.269	6.861	
benzene	4.996	0.004	2.412	0.252	9.382	
THF	5.114	0.024	2.893	0.262	10.494	
J1 shale:						
Original shale	6.399	0.064	2.974	0.257	1.700	
After extraction with:						
acetone	6.731	0.011	20.006	0.232	1.654	
CS_2	9.573	0.172	16.903	0.308	1.997	
benzene	5.063	0.012	18.416	0.237	2.012	
THF	0.000	0.253	22.122	0.335	1.492	
LH10 shale:						
Original shale	7.167	0.103	3.122	0.298	2.897	
After extraction with:						
acetone	10.632	0.101	3.500	0.270	2.655	
CS_2	8.381	0.092	3.371	0.268	2.933	
benzene	2.466	0.228	3.000	0.352	2.859	
THF	7.667	0.119	4.041	0.289	2.780	
H317 shale						
Original shale	8.347	0.068	3.259	0.272	1.686	
After extraction with:						
acetone	0.000	0.627	2.844	0.858	2.181	
CS_2	5.472	0.066	3.749	0.243	2.129	
benzene	0.000	0.268	2.313	0.485	2.031	
THF	0.000	0.3420	3.753	0.551	1.624	

¹⁵⁵ The integrated peak areas were used to calculate FTIR ratios.

[#] AR1=0 for residues because aromatic bands (δ Ar C=C, ν Ar C-H) were not present in the FTIR spectrum.

5 Discussions

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5.1 The influence of solvents on extraction yield and composition of the soluble mixture

Previous studies have found that the extraction yields of shale and the composition of the soluble mixture are related to the properties of the solvent, extraction temperature, the geochemical parameters of the shale, and so on (Hu et al., 1999; Olukcu et al., 1999; Shaohui et al., 2000; Abourriche et al., 2013; Cao et al., 2019). As the polarity of the solvent increases, the extraction yield increases accordingly (Masaki et al., 2004). The solvent dissolution capacity has obvious temperature dependence, and the dissolution capacity increases with the increase of temperature (Hu et al., 1999). The increase in extraction pressure and temperature will promote the activation energy of the sample (Allawzi et al., 2011).

The Hansen solubility parameters of the four solvents are shown in Table 5, the extraction ability of CS₂ is similar to that of benzene (Table 5). Because of the aromatic structure, high boiling point, and strong polarity, THF could have a stronger extraction ability than other solvents (Table 5).

	1 1			`	,	
Solvent	Hansen solubility parameters			_ Polarity	Boiling point	Aromaticity
	Dispersion	Polarity	H-bond	·		·
THF	16.8	5.7	8	4.2	65 °C	Aromatic
CS_2	20.2	0	0.6	0.15	46.5 °C	Non-aromatic
Acetone	15.5	10.4	7	5.4	56 °C	Non-aromatic
Benzene	18.4	0	2	3	80 °C	Aromatic

Table 5. The properties of the four solvents (Cao et al., 2020)

Allawzi et al. (2011) found that the OM obtained by solvent extraction is mainly composed of low molecular weight compounds (e.g., saturated hydrocarbons, olefin hydrogen, aromatic compounds). Our results show that the extraction yield of shale with THF is significantly higher than that of other solvents (Fig. 4a), which could be attributed to that a mass of the heaviest macromolecular compound-asphaltene was screened out (Cao et al., 2020). The significant elimination of OM (i.e., asphaltene) by THF may be related to the properties of the THF, including the aromatic structure (Johnson et al., 1967), high boiling point (Cao et al., 2019), excellent Hansen solubility parameters and strong polarity (Toolan et al., 2016) (Table 5), which could assist to destroy the interact between shale matrix and the asphaltenes (i.e., a complex molecular architecture with a central polycyclic aromatic hydrocarbon (PAH) with peripheral alkane substituents) (Schuler et al., 2017) of PAH molecular polymerization (Schuler et al., 2015).

The extraction yields of the studied samples are in the order of LH10, JH2, H317, and J1 regardless of solvents (Fig. 4a), which may be due to the soluble hydrocarbon content (S₁) of the studied sample (Table 2). According to the TOC-

normalized yield of extracts, the mature samples J1 (T_{max} 449°C) had significantly higher extractables than other samples (Fig. 4b), which may be related to that the J1 sample (T_{max} 449°C) was at the peak of hydrocarbon generation, thus a large number of kerogens were cracked into oil and bitumen (Ertas et al., 2006; Wei et al., 2014). However, a little kerogen was converted to a small amount of oil in the early maturity stage (Cao et al., 2020), so the TOC-normalized extraction yield of the JH2 sample is low. However, the TOC-normalized extraction yield of late mature shale H317 is similar to that of early mature shale JH2, which could be attributed to that some of the oil is cracked to natural gas or transported to other locations with maturation (Cao et al., 2020).

5.2 Effect of solvent extraction on the chemical structure of shales

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The application of FTIR spectroscopy provides an evaluation of the aromaticity and length of aliphatic chains for original shales and residues from extractions. Table 4 showed that the aromaticity (AR2 and AR3) of original shale OM with different maturity is obviously different ranging from 2.828 to 3.327. Fig. 7 shows there is a positive correlation between aromaticity and maturity in shale (Feng et al., 2013). Thus, the above-mentioned facts indicate that the thermal maturation can increase the aromaticity of shale OM.

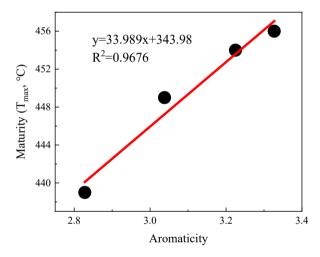


Fig. 7. Relationships between the aromaticity and the maturity in shale OM.

Table 4 showed the length of aliphatic chains (LAC) from late mature shale (i.e., LH10 and H317) is higher than those of mature shale J1 and marginally mature shale JH2. In addition, the LAC of the early mature shale J1 is also higher than the marginally mature shale JH2 (Table 4). However, the LAC of the higher mature H317 shale (T_{max}=456°C) is lower than that of mature LH10 shale (T_{max}=454°C). Those indicate that the aliphatic chains lengthened with the increase of maturity before the late maturity stage (Feng et al., 2013), and then shortened as the maturity further increases. That may be attributed to the fact that kerogen cracking to form a large amount of bitumen at the low maturity stage leads to longer aliphatic chains with increasing maturity, while at the high maturity stage bitumen is largely consumed, the OM represented by bitumen is further

cracked, thus shortening the aliphatic chains with increasing maturity (Feng et al., 2013). However, previous studies have also observed that aliphatic chains lengthened become monotonically shorter and/or more branched with maturity, which indicates that longer aliphatic chains can be preferentially cleaved. The cleavage of the C–C bonds between carbons α and β to a ring could explain this result (Lin and Ritz, 1993). Moreover, the large differences in the sources of OM in different regions may be the cause of the above contradictions.

The DOS of aromatic rings represents the fraction of aromatic sites where hydrogen atoms are substituted by alkyl groups, there is no regularity in the DOS (i.e., the fraction of aromatic sites where hydrogen atoms are substituted by alkyl groups) of different maturity shales (Table 4), therefore the fraction of aromatic sites where hydrogen atoms are substituted by alkyl groups in shale is independent of maturity.

In addition, the FTIR-derived LAC values smaller than 1 show the superiority of CH₃ bands (i.e., asymmetric stretching vibration) in shales corresponding to short and branched aliphatic chains (Furmann et al., 2013). Our results demonstrate that aliphatic chains are shorter with higher branched in the original shale samples, which could not be changed during the extractions (Table 4). In addition, the FTIR of shales after different solvent extractions is irregular, which may be influenced by the inorganic minerals. Therefore, it seems much more reasonable to conclude that FTIR was unable to detect any significant change in the LAC values due to solvent extraction. Furthermore, the aromaticity (both AR2 and AR3) of residues after THF extractions is significantly higher than those after other solvents extraction (Table 4), which may be related to that THF only dissolves relatively fewer aromatic hydrocarbons from shales (Cao et al., 2020) and the residual abundant aromatic hydrocarbons in shale benefits OM aromaticity (Monger, 1984).

6 Conclusions

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Soxhlet-extractions with THF, benzene, CS₂, and acetone respectively have been applied to the shale samples with a progressive maturation gradient in order to gain insights into the proportion of soluble hydrocarbon and the chemical characteristics of shale with different maturity. The following conclusions have been obtained:

- The extraction yield of shale with THF is significantly higher than that of other solvents, which may be related to the properties of the THF, including the aromatic structure, high boiling point, excellent Hansen solubility parameters, and strong polarity. The TOC-normalized yield of the mature sample J1 is significantly higher than that of other samples, which may be related to that the J1 sample is at the peak of hydrocarbon generation, thus a large number of kerogens were cracked into oil and bitumen.
- 230 2 Thermal maturation of shales can increase the aromaticity of OM. The aliphatic chains in the shale OM lengthened with the increase of maturity before late maturity stage, and then shortened with the further increase of maturity in late maturity stage.
 - 3 The extraction of shales with solvents hardly changes the length of aliphatic chains. Higher aromaticity is observed in shale residues after THF extractions than other solvents (i.e., acetone, CS₂, benzene).

Author contributions. Yan Cao was responsible for the conceptualization and methodology of the study, carrying out the experiments, compilation and analysis of data, and writing the paper. Zhijun Jin was responsible for the acquisition and management of financial support, contribution to experimental design. Rukai Zhu and Kouqi Liu investigated and revised the ideas of the article. All authors contributed to the review of the manuscript.

240 Competing interests. The contact author has declared that none of the authors has any competing interests.

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