## Supplement of

## Bacteria in clouds biodegrade atmospheric formic and acetic acids

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**Table S1.** Irreversible processes in the aqueous phase. The kinetic data are the same as used in the model study by Khaled et al. (2021). The biodegradation rate constants are calculated based on the lab data by Vaïtilingom et al. (2011).

Chemical reactions					
	Reactants		Products	$k [M^{-1} s^{-1}]$	$E_a/R[K]$
R1	$SO_2 + O_3$	$\rightarrow$	$S(VI) + O_2$	$2.4 \cdot 10^4$	
R2	$HSO_3^- + O_3$	$\rightarrow$	$S(VI) + O_2$	$3.7 \cdot 10^5$	5530
R3	$SO_3^{2-} + O_3$	$\rightarrow$	$S(VI) + O_2$	$1.5 \cdot 10^9$	5280
R4	$H_2O_2 + HSO_3^- + H^+$	$\rightarrow$	$S(VI) + H_2O$	$7.2 \cdot 10^7 \text{ M}^{-2} \text{ s}^{-1}$	4000
R5	$HO_2 + HO_2$	$\rightarrow$	$H_2O_2 + O_2$	$8.3 \cdot 10^5$	2720
R6	$O_2^-$ + HO <sub>2</sub>	$\rightarrow$	$H_2O_2 + O_2$	$9.7 \cdot 10^7$	1060
R7	$OH + CH_2(OH)_2$	$\rightarrow$	$HO_2 + HCOOH$	$1 \cdot 10^{9}$	1000
R8	$OH + CH_3OOH$	$\rightarrow$	$CH_3O_2 + H_2O$	$2.4 \cdot 10^7$	1680
R9	$OH + CH_3OOH$	$\rightarrow$	$HO_2 + HCOOH$	$61 \cdot 10^{6}$	1680
R10	$O_3 + O_2^- (+ H^+)$	$\rightarrow$	$OH + 2 O_2$	$1.5 \cdot 10^9$	2200
R11	OH + CHOCHO	$\rightarrow$	$HO_2 + CHOCOOH$	$1.1 \cdot 10^9$	1516
R12	OH + CHOCOOH	$\rightarrow$	$HO_2 + H_2C_2O_4$	$3.6 \cdot 10^8$	1000
R13	$OH + CHOCOO^{-}$	$\rightarrow$	$HO_2 + H_2C_2O_4$	$2.9 \cdot 10^9$	4300
R14	$OH + C_2 O_4^{2-}$	$\rightarrow$	$O_2^- + 2 CO_2 + OH^-$	$1.6 \cdot 10^8$	4300
R15	$OH + HC_2O_4^-$	$\rightarrow$	$HO_2 + 2 CO_2 + OH^-$	$1.9 \cdot 10^8$	2800
R16	$OH + H_2C_2O_4$	$\rightarrow$	$HO_2 + 2 CO_2 + H_2O$	$1.4 \cdot 10^{6}$	
R17	$OH + CH_3C(O)COO^-$	$\rightarrow$	$HO_2 + CO_2 + CH_3COO^-$	$7.2 \cdot 10^8$	
R18	$OH + CH_3C(O)COOH$	$\rightarrow$	$HO_2 + H_2O + CH_3COOH$	$1.2 \cdot 10^8$	
R19	$OH + CH_3CHO$	$\rightarrow$	$HO_2 + CO_2 + CH_3COOH$	$3.6 \cdot 10^9$	
R20	$OH + CH_3C(O)CHO$	$\rightarrow$	$HO_2 + CHC(O)COOH$	$1.1 \cdot 10^9$	1516
R21	$OH + HCOO^{-}$	$\rightarrow$	$HO_2 + CO_2 + H_2O$	$3.2 \cdot 10^9$	1000
R22	OH + HCOOH	$\rightarrow$	$HO_2 + CO_2 + H_2O$	$1.3 \cdot 10^8$	1000
R23	$CH_3O_2 + CH_3O_2$	$\rightarrow$	$CH_2O + CH_3OH + HO_2$	$1.7 \cdot 10^8$	2200
R24	$H_2O_2 + OH$	$\rightarrow$	$HO_2 + H_2O$	$3 \cdot 10^{7}$	1680
R25	OH + WSOC	$\rightarrow$	WSOC + $HO_2$	$3.8 \cdot 10^8$	
R26	$OH + CH_2OHCHO$	$\rightarrow$	$CH_2OHCOOH + HO_2$	$1.2 \cdot 10^9$	
R27	$OH + CH_2OHCOOH$	$\rightarrow$	$CHOCOOH + HO_2$	$5.4 \cdot 10^8$	
R28	$OH + CH_2OHCOO^-$	$\rightarrow$	CHOCOOH + $HO_2$	$1.2 \cdot 10^9$	
R29	$OH + CH_3COOH$	$\rightarrow$	0.85 CHOCOOH + $0.15$ HCHO + HO <sub>2</sub>	$1.5 \cdot 10^7$	1330
R30	$OH + CH_3COO^-$	$\rightarrow$	0.85 CHOCOOH + $0.15$ HCHO + HO <sub>2</sub>	$1 \cdot 10^{8}$	1800
R31	$CH_3(O)O_2 + O_2^-$	$\rightarrow$	CH <sub>3</sub> COOH	$1 \cdot 10^{9}$	
R32	$CH_3(O)O_2 + CH_3(O)O_2$	$\rightarrow$	$2 \mathrm{CH}_3\mathrm{O}_2$	$1.5 \cdot 10^8$	
Biodegradation				$k_{bact}$ [L cell <sup>-1</sup> s <sup>-1</sup> ]	
R33	HCOOH/HCOO <sup>-</sup> + Bacteria	$\rightarrow$	Products	$1.5 \cdot 10^{-13}$	
R34	CH <sub>3</sub> COOH/CH <sub>3</sub> COO <sup>-</sup> + Bacteria	$\rightarrow$	Products	$8.7 \cdot 10^{-14}$	

				K <sub>a</sub> [M]
E1	$H_2O$	$\rightleftharpoons$	$OH^-+H^+$	$1.0 \cdot 10^{-14}$
E2	$HO_2$	$\rightleftharpoons$	${\rm O_2}^-$ + ${\rm H^+}$	$1.60 \cdot 10^{-5}$
E3	CHOCOOH	$\rightleftharpoons$	$CHOCOO^{-} + H^{+}$	6.60·10 <sup>-4</sup>
E4	HCOOH	$\rightleftharpoons$	$HCOO^- + H^+$	$1.77 \cdot 10^{-4}$
E5	$H_2C_2O_4$	$\rightleftharpoons$	$HC_2O_4^- + H^+$	$6.40 \cdot 10^{-2}$
E6	$\mathrm{HC_2O_4}^-$	$\rightleftharpoons$	$C_2O_4^{2-} + H^+$	$5.25 \cdot 10^{-5}$
E7	$HNO_3$	$\rightleftharpoons$	$NO_{3}^{-} + H^{+}$	22
E8	$SO_2 \cdot H_2O$	$\rightleftharpoons$	$HSO_3^- + H^+$	0.013
E9	$HSO_3^-$	$\rightleftharpoons$	$SO_3^{2-} + H^+$	6.60·10 <sup>-8</sup>
E10	$H_2SO_4$	$\rightleftharpoons$	$HSO_4^- + H^+$	1000
E11	$\mathrm{HSO_4}^-$	$\rightleftharpoons$	$SO_4{}^{2-} + H^+$	0.102
E12	$NH_3$	$\rightleftharpoons$	$\mathrm{NH_4^+}$ + $\mathrm{OH^-}$	$1.76 \cdot 10^{-5}$

Table S2. Aqueous phase equilibria. The data are the same as used in the model study by Khaled et al. (2021).

**Table S3.** Phase transfer parameters. The parameters are the same as used in the model study by Khaled et al. (2021). The Henry's law constant for acetic acid is the same as used by Brimblecombe and Clegg (1988), its  $\alpha$  and  $D_g$  values are estimated to be same as for similar compounds.

Species	$M_g$	α	$D_g$	K <sub>H</sub>
	$[g \text{ mol}^{-1}]$		$[\text{cm}^2 \text{ s}^{-1}]$	$[M atm^{-1}]$
O <sub>3</sub>	48	0.05	0.148	$1.14 \cdot 10^{-2}$
$H_2O_2$	34	0.1	0.118	$1.02 \cdot 10^5$
OH	17	0.05	0.153	25
$HO_2$	33	0.05	0.104	$9.10^{3}$
HCHO	30	0.02	0.164	$4.99 \cdot 10^3$
$CH_3O_2$	47	0.0038	0.135	310
$CH_3OOH$	48	0.0038	0.135	310
$HNO_3$	63	0.054	0.132	$2.1 \cdot 10^5$
$N_2O_5$	108	0.0037	0.110	1.4
$SO_2$	64	0.035	0.128	1.23
HCOOH	46	0.012	0.153	5530
$(CHO)_2$	58	0.023	0.115	$4.19 \cdot 10^5$
CH <sub>3</sub> COCHO	72	0.1	0.115	$3.2 \cdot 10^4$
$NH_3$	17	0.1	0.1	60.7
CH <sub>3</sub> COOH	60	0.1	0.1	5500

Table S4. Gas phase formation and loss processes of formic and acetic acids. The full gas phase mechanism is the same as used in Barth et al. (2021).

	Reactants		Products	$k [cm^3 s^{-1}]$	$E_a/R[K]$
Rg1	Isoprene + $O_3$	$\rightarrow$	0.2 CH <sub>3</sub> COOH + 0.1 OH + 0.27 HO <sub>2</sub> +	9.6·10 <sup>-18</sup>	
			$0.06 \text{ HO}_2 + 0.6 \text{ HCHO} + \text{CH}_3\text{COOH} +$		
			0.4 MACR + 0.3 MVK + 0.07 C <sub>3</sub> H <sub>6</sub> +		
			0.2 CH <sub>3</sub> (O)O <sub>2</sub>		
Rg2	$CH_3(O)O_2 + HO_2$	$\rightarrow$	$0.1 O_3 + 0.7 CH_3C(O)OOH + 0.3$	$1.8 \cdot 10^{-11}$	360
			CH <sub>3</sub> COOH		
Rg3	HCOOH + OH	$\rightarrow$	$CO_2 + H_2O + HO_2$	$1.5 \cdot 10^{-12}$	
Rg4	$CH_3COOH + OH$	$\rightarrow$	$0.7 \text{ OH} + 0.7 \text{ CH}_3 \text{CHO} + 0.3 \text{ C}_2 \text{H}_5 \text{O}_2$	$1 \cdot 10^{-11}$	200

**Table S5.** Initial mixing ratios of gas phase species [ppb] and concentrations of aqueous phase species [ $\mu g m_{air}^{-3}$ ]; all other species are not initialized

Gas phase species	Mixing ratio [ppb]
O <sub>3</sub>	60
$H_2O_2$	1
НСНО	0.1
HCOOH	0.5
CH <sub>3</sub> COOH	0.2
$HNO_3$	1
$SO_2$	2
$NH_3$	1
NO	3
$NO_2$	0.1
CO	150
Isoprene	1
Toluene	2
Ethylene	0.5
$CH_4$	1850 (const.)
Aqueous phase species	Concentration
WSOC	$20 \ \mu M$
Bacteria cells	$0.1 \ \mathrm{cm}_{air}^{-3}$

**Table S6.** Rates for all processes shown in Figure 6, at the end of 1-hour simulation time and for  $D_d = 20 \ \mu$ m. The upper part of the table lists the rates in units of  $10^{-16} \ \text{mol g}_{air}^{-1} \ \text{s}^{-1}$ . These numbers allow the comparison of rates related scaled by the aqueous phase volumes. The bottom part of the table reports the same rates (only aqueous phase) in units of  $10^{-9} \ \text{mol L}_{aq}^{-1} \ \text{s}^{-1}$ . These units allow comparing the two droplet classes. If the chemical composition were identical in both classes, the rates should be identical, too. Any deviation is caused by the biodegradation in drop class 2.

Acid	pН	$PT_1$	$S_{aq1}$	$L_{aq1}$	$PT_2$	$S_{aq2}$	$L_{aq2}$	$L_{Bact}$	$S_g$	$L_g$
		$10^{-16} \text{ mol } g_{air}^{-1} \text{ s}^{-1}$								
Formic acid	3	-2.5	2.9	-0.45	0.87	0.003	-4.10-4	-0.87	0	-0.77
	4.6	3.7	5.3	14	2.0	0.006	-0.011	-2.0	0	-0.22
	5.6	1.2	11	27	0.49	0.013	-0.008	-0.5	0	-0.015
Acetic acid	3	-3.0	3.1	-0.004	0.15	0.003	-3.5.10-6	-0.15	0.38	-6.4
	4.6	-8.2	8.9	-0.05	0.31	0.009	-5·10 <sup>-5</sup>	-0.32	0.85	-5.4
	5.6	-10	16	-0.74	0.98	0.02	-7.10-4	-1.0	1.1	-3.4
			10-9	mol $L_a^-$	$q^{1} s^{-1}$					
Formic acid	3	-0.61	0.72	-0.11	210	0.72	-0.11	-210		
	4.6	0.91	1.3	-3.5	500	1.4	-2.8	-500		
	5.6	0.3	2.8	-6.6	120	3.1	-2.0	-120		
Acetic acid	3	-0.74	0.76	-8.7·10 <sup>-4</sup>	37	0.76	-8.5·10 <sup>-4</sup>	-38		
	4.6	-2.0	2.2	-0.012	77	2.2	-0.012	-79		
	5.6	-2.5	4.0	-0.18	240	4.6	-0.17	-250		



**Figure S1.** Results from 900 1-hour simulations (30 pH values, 30 drop diameters, Total formic acid concentrations (gas + aqueous) and absolute concentration difference ( $(c_0 - c_t)$  in the absence of bacteria (a, c) and in the presence of bacteria (b, d). e) Relative difference in concentration due to bacteria according to Equation 6. The threshold of  $c_0 - c_{t,nocell}$  in panel e) is chosen to avoid displaying very high values by dividing by an irrelevant small concentration difference



**Figure S2.** Results from 900 1-hour simulations (30 pH values, 30 drop diameters, Total acetic acid concentrations (gas + aqueous) and absolute concentration difference ( $(c_0 - c_t)$  in the absence of bacteria (a, c) and in the presence of bacteria (b, d). e) Relative difference in concentration due to bacteria according to Euqation 6

## References

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