# **Compilation of Henry's law constants (version 5.0.0) for water as solvent**

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**Abstract.** Many atmospheric chemicals occur in the gas phase as well as in liquid cloud droplets and aerosol particles. Therefore, it is necessary to understand their distribution between the phases. According to Henry's law, the equilibrium ratio between the abundances in the gas phase and in the aqueous phase is constant for a dilute solution. Henry's law constants of trace gases of potential importance in environmental chemistry have been collected and converted into a uniform format. The compilation

5 contains 46434 values of Henry's law constants for 10173 species, collected from 994 references. It will also be is also available on the internet at https://www.henrys-law.org. This article is a living review that supersedes the now obsolete publication by Sander (2015).

#### 1 Introduction

Henry's law is named after the English chemist William Henry, who studied the topic in the early 19th century. In his publicationabout the quantity of gases absorbed by water (Henry, 1803), he described the results of his experiments:

"[...] water takes up, of gas condensed by one, two, or more additional atmospheres, a quantity which, ordinarily compressed, would be equal to twice, thrice, &c. the volume absorbed under the common pressure of the atmosphere."

In other words, the amount of dissolved gas is proportional to its partial pressure in the gas phase. The proportionality factor is called a Henry's law constant. In atmospheric chemistry, these constants are needed to describe the distribution exchange of trace species between the air and liquid cloud dropletsor aerosol particles, aerosol particles, oceans and other bodies of water. In other areas of environmental research, the constants are needed to calculate the vaporization of contaminants, e.g., from rivers and during waste water treatment (e.g. Shen, 1982; Hawthorne et al., 1985; David et al., 2000).

Section 2 provides theoretical background about Henry's law and commonly used quantities and units. In Sect. 3, the compilation of Henry's law constants is described in detail. Additional information can be found in the electronic supplement, which is described in Sect. 4.

Table 1.	Variants	of Henry	's law	constants	H.
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symbol	definition <sup>a</sup>	SI unit	other commonly used (non-SI) units $^{b}$	conversion <sup><math>c</math></sup> from $H_s^{cp}$
Henry's law solubility constants $H_s$				
$H_{\rm s}^{cp}$	$c_{\rm a}/p$	$ m molm^{-3}Pa^{-1}$	$M  atm^{-1}$	
$H_{\rm s}^{xp}$	x/p	$\mathrm{Pa}^{-1}$	$\mathrm{atm}^{-1}$	$H_{\rm s}^{xp}=H_{\rm s}^{cp}\times M_{\rm H_2O}/\varrho_{\rm H_2O}$
$H_{\rm s}^{bp}$	b/p	$\rm molkg^{-1}Pa^{-1}$	$\mathrm{molkg}^{-1}\mathrm{atm}^{-1}$	$H_{\rm s}^{bp}=H_{\rm s}^{cp}/\varrho_{\rm H_2O}$
$H_{\rm s}^{cc}$	$c_{\rm a}/c_{\rm g}$	1 (dimensionless)		$H_{\rm s}^{cc}=H_{\rm s}^{cp}\times RT$
Henry's law volatility constants $H_v$				
$H_{\rm v}^{pc}$	$p/c_{\mathrm{a}}$	${\rm Pa}{\rm m}^3{\rm mol}^{-1}$	$\rm atmm^3mol^{-1}$	$H_{\rm v}^{pc}=1/H_{\rm s}^{cp}$
$H_{\rm v}^{px}$	p/x	Pa	atm	$H_{\rm v}^{px} = (\varrho_{\rm H_2O}/M_{\rm H_2O})/H_{\rm s}^{cp}$
$H^{pw}_{\rm v}$	p/w	Pa	atm	$H_{\rm v}^{pw} = (\varrho_{\rm H_2O}/M_B)/H_{\rm s}^{cp}$
$H_{\rm v}^{cc}$	$c_{ m g}/c_{ m a}$	1 (dimensionless)		$H_{\rm v}^{cc} = 1/(H_{\rm s}^{cp} \times RT)$

<sup>a</sup> The definitions apply only at equilibrium and in the limit of infinite dilution.

<sup>b</sup> Here,  $M = mol L^{-1}$  and atm = 101325 Pa.

<sup>*c*</sup> Here,  $M_{\rm H_2O}$  and  $\rho_{\rm H_2O}$  are the molar mass and density of water, respectively.  $M_B$  is the molar mass of the solute. The simplified conversion formulas are valid only for binary solutions and ideal gases. More conversion formulas can be found in Tab. 2 of Sander et al. (2022).

This article is a living review describing version  $5.0.0^1$ . Compared to the now obsolete version 4.0 (Sander, 2015), the compilation contains 29084 additional values of Henry's law constants for 5541 additional species, collected from 305 additional references. In cases where experimental data are available for a large temperature range, the <u>data-values</u> were refitted to a

25 3-parameter equation , replacing in addition to the 2-parameter fits that were used previously. The symbols of the Henry's law constants have been adjusted in order to follow the new recommendations of the International Union of Pure and Applied Chemistry (IUPAC) by Sander et al. (2022). In addition to the CAS registry numbers, chemical species are now also identified by their InChIKeys (Heller et al., 2015).

#### 2 Theoretical background

#### 30 2.1 Fundamental types of Henry's law constants

There are many variants of Henry's law constants which can all be classified into two fundamental types: One possibility is to put the aqueous phase into the numerator and the gas phase into the denominator, i.e., define the constant as the quotient A/G. Here, A and G are quantities describing the equilibrium composition (at infinite dilution) of the aqueous phase and

<sup>&</sup>lt;sup>1</sup>The name of this version indicates that it is a "release candidate" used for the interactive discussion in ACPD. If necessary, corrections can still be made. It is planned to release the final version 5.0.0 together with the final paper in ACP.

the gas phase, respectively. Alternatively, the Henry's law constant can be defined as the quotient G/A, which results in

the inverse value. There is no advantage or disadvantage in using one or the other, the two types exist purely for historical reasons. Unfortunately, the name "Henry's law constant" is used for both types. Therefore, expressions like "a large Henry's law constant" are meaningless unless the type is specified. Especially the dimensionless constants are very error-prone because their type cannot be deduced from the unit. In order to have a consistent terminology, the name "Henry's law solubility constant" (or "Henry solubility" for conciseness) should be used when refering to *A*/*G*. When refering to *G*/*A*, the name "Henry's law
volatility constant" (or "Henry volatility") should be used.

#### 2.2 Variants of Henry's law constants

For both of the fundamental types described in the previous section, there are several variants. This results from the multiplicity of quantities that can be chosen to describe the composition of the two phases. Typical choices for the aqueous phase are molar concentration  $(c_a)$ , molality (b), and amount fraction (x). For the gas phase, molar concentration  $(c_g)$  and partial pressure (p)

45 are often used. Note, however, that it is not possible to use the gas-phase amount fraction (y). At a given gas-phase amount fraction, the aqueous-phase concentration  $c_a$  depends on the total pressure and thus the ratio  $y/c_a$  is not a constant.

There are numerous combinations of these quantities. The eight variants recommended by IUPAC are summarized in Table 1. Numerical values of conversion factors between them are shown in Tables 2, 3, and 4.

#### 2.3 Symbols

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50 In the current literature, a plethora of different symbols is used for the Henry's law constants. Several symbols are used for the same variant, and sometimes the same symbol is used for different variants. However, for this work a consistent terminology is indispensable. Here, the IUPAC recommendations by Sander et al. (2022) are used: For Henry's law solubility constants, the symbol  $H_s$  is used, and for Henry's law volatility constants the symbol  $H_v$  is used.

To specify the exact variant of the Henry's law constant, two superscripts are used. They refer to the numerator and the 55 denominator of the definition. For example,  $H_s^{cp}$  refers to the Henry solubility defined as c/p. If  $H_s$  refers to the reference temperature  $T^{\ominus} = 298.15$  K, it will be denoted as  $H_s^{\ominus}$ . A summary of the symbols is shown in Table 5.

#### 2.4 Temperature dependence of Henry's law constants

In spite of the name Henry's law "*constant*", it should be kept in mind that its value still depends on some parameters, e.g., the temperature *T*. The temperature dependence of equilibrium constants can be described with the van't Hoff equation, which also applies to Henry's law:

$$\frac{\mathrm{d\ln}H_{\mathrm{s}}}{\mathrm{d}(1/T)} = \frac{-\Delta_{\mathrm{sol}}H}{R},\tag{1}$$

**Table 2.** Conversion factors between several Henry's law solubility constants  $H_s$  (at  $T^{\ominus} = 298.15$  K and  $\varrho^{\ominus} = 997$  kg/m<sup>3</sup>). For example, the second table entry indicates that  $H_s^{cp} = 1 \text{ mol m}^{-3} \text{ Pa}^{-1} \Leftrightarrow H_s^{cp} = 101.325 \text{ M atm}^{-1}$ .

_	$H_{\rm s}^{cp} = \dots \frac{{ m mol}}{{ m m}^3  { m Pa}}$	$H_{\rm s}^{cp} = \dots \frac{{\rm M}}{{ m atm}}$	$H_{\rm s}^{cc} = \dots$	$H_{\rm s}^{bp} = \dots \frac{{ m mol}}{{ m kg Pa}}$	$H_{\rm s}^{bp} = \dots \frac{{ m mol}}{{ m kg}{ m atm}}$	$H_{\rm s}^{xp} = \dots \frac{1}{{ m atm}}$	$\alpha = \dots$
$H_{\rm s}^{cp} = 1 \frac{ m mol}{ m m^3 Pa}$	1.00000	101.325	2478.96	$1.00301 \times 10^{-3}$	101.630	1.83089	2271.10
$H_{\rm s}^{cp} = 1 \ \frac{\rm M}{\rm atm}$	$9.86923 \times 10^{-3}$	1.00000	24.4654	$9.89893 \times 10^{-6}$	1.00301	0.0180695	22.4140
$H_s^{cc} = 1$	$4.03395 \times 10^{-4}$	0.0408740	1.00000	$4.04609 \times 10^{-7}$	0.0409970	$7.38573 \times 10^{-4}$	0.916150
$H_{\rm s}^{bp} = 1 \ \frac{\rm mol}{\rm kg  Pa}$	997.000	$1.01021\times 10^5$	$2.47152\times10^{6}$	1.00000	$1.01325\times10^5$	1825.40	$2.26428\times10^6$
$H_{\rm s}^{bp} = 1 \ \frac{\rm mol}{\rm kg  atm}$	$9.83962 \times 10^{-3}$	0.997000	24.3920	$9.86923 \times 10^{-6}$	1.00000	0.0180153	22.3467
$H_s^{xp} = 1 \ \frac{1}{\text{atm}}$	0.546182	55.3419	1353.96	$5.47826 \times 10^{-4}$	55.5084	1.00000	1240.43
<i>α</i> = 1	$4.40316 \times 10^{-4}$	0.0446150	1.09152	$4.41641 \times 10^{-7}$	0.0447493	$8.06171 \times 10^{-4}$	1.00000

**Table 3.** Conversion factors between several Henry's law volatility constants  $H_v$  (at  $T^{\ominus} = 298.15$  K and  $\varrho^{\ominus} = 997$  kg/m<sup>3</sup>). For example, the second table entry indicates that  $H_y^{px} = 1$  atm  $\Leftrightarrow H_y^{pc} = 1.83089$  m<sup>3</sup> Pa mol<sup>-1</sup>.

	$H_{v}^{px} = \dots \operatorname{atm}$	$H_{\rm v}^{pc} = \dots \frac{{ m m}^3  { m Pa}}{{ m mol}}$	$H_{\rm v}^{pc} = \dots \frac{{ m m}^3{ m atm}}{{ m mol}}$	$H_{v}^{cc} = \dots$
$H_{\rm v}^{px} = 1$ atm	1.00000	1.83089	$1.80695 \times 10^{-5}$	$7.38573  imes 10^{-4}$
$H_v^{pc} = 1 \frac{\mathrm{m}^3 \mathrm{Pa}}{\mathrm{mol}}$	0.546182	1.00000	$9.86923  imes 10^{-6}$	$4.03395  imes 10^{-4}$
$H_{\rm v}^{pc} = 1 \ \frac{{ m m}^3  { m atm}}{{ m mol}}$	55341.9	$1.01325 \times 10^{5}$	1.00000	40.8740
$H_{\rm v}^{cc} = 1$	1353.96	2478.96	0.0244654	1.00000

**Table 4.** Products of Henry's law solubility constants  $H_s$  and Henry's law volatility constants  $H_v$  (at  $T^{\ominus} = 298.15$  K and  $\varrho^{\ominus} = 997$  kg/m<sup>3</sup>). For example, if  $H_v^{px} = 5$  atm, then  $H_s^{bp} \approx 11 \text{ mol}/(\text{kg atm})$  because  $5 \times 11 \approx 55.5084$ .

	$\frac{H_{\rm s}^{cp}}{\rm mol/(m^3Pa)}$	$\frac{H_{\rm s}^{cp}}{{\rm M/atm}}$	$\frac{H_{\rm s}^{cc}}{1}$	$\frac{H_{\rm s}^{bp}}{\rm mol/(kgPa)}$	$\frac{H_{\rm s}^{bp}}{{\rm mol}/({\rm kgatm})}$	$\frac{H_{\rm s}^{xp}}{1/{\rm atm}}$	$\frac{\alpha}{1}$
$\frac{H_{\rm v}^{px}}{\rm atm}$	0.546182	55.3419	1353.96	$5.47826  imes 10^{-4}$	55.5084	1.00000	1240.43
$\frac{H_{\rm v}^{pc}}{{\rm m}^3{\rm Pa/mol}}$	1.00000	101.325	2478.96	$1.00301 \times 10^{-3}$	101.630	1.83089	2271.10
$\frac{H_{\rm v}^{pc}}{{\rm m}^3{\rm atm/mol}}$	$9.86923  imes 10^{-6}$	$1.00000 \times 10^{-3}$	0.0244654	$9.89893  imes 10^{-9}$	$1.00301 \times 10^{-3}$	$1.80695 \times 10^{-5}$	0.0224140
$\frac{H_{\rm v}^{cc}}{1}$	$4.03395 \times 10^{-4}$	0.0408740	1.00000	$4.04609 \times 10^{-7}$	0.0409970	$7.38573 \times 10^{-4}$	0.916150

where  $\Delta_{sol}H =$  enthalpy of dissolution and R = gas constant. Note that the letter H in the symbol  $\Delta_{sol}H$  refers to enthalpy and is not related to the letter H for Henry's law constants. Integrating the above equation leads to

$$\ln H_{\rm s} = \frac{-\Delta_{\rm sol}H}{R} \frac{1}{T} + const\tag{2}$$

65 Calling the constant of integration A, and defining the parameter  $B = -\Delta_{sol}H/R$ , we get:

$$\ln H_{\rm s} = A + \frac{B}{T} \tag{3}$$

or

$$H_{\rm s} = \exp\left(A\right) \times \exp\left(\frac{B}{T}\right) \tag{4}$$

To determine the parameters A and B experimentally, Henry's law constants are measured at several temperatures, and the 70 method of least squares is used to fit the points to a function. Note that functions (3) and (4) produce slightly different fit parameters because the logarithmic function (3) puts less weight on errors of large Henry's law constants than the linear function (4) does. In this work, linear regression is performed using Eq. (3).

Thermodynamic data are often available at the temperature  $T^{\ominus} = 298.15$  K. To present Henry's law constants at  $T^{\ominus}$  and also show their temperature dependence, an alternative form of Eq. (4) can be used:

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$$H_{\rm s} = H_{\rm s}^{\ominus} \times \exp\left(B\left(\frac{1}{T} - \frac{1}{T^{\ominus}}\right)\right).$$
 (5)

symbol	quantity	SI unit*
Q	density	$\mathrm{kg}\mathrm{m}^{-3}$
A	parameter for the temperature dependence of $H_s$	1
b	molality	$ m molkg^{-1}$
В	parameter for the temperature dependence of $H_s$	<b>∔</b> K
C	parameter for the temperature dependence of $H_s$	1
$c_{\rm a}$	aqueous-phase concentration	$ m molm^{-3}$
$c_{ m g}$	gas-phase concentration	$ m molm^{-3}$
D	parameter for the temperature dependence of $H_s$	$+K^{-1}$
$\Delta_{sol}G$		$\mathrm{Jmol^{-1}}$
	free energy of dissolution	
$\Delta_{\rm sol} H$	molar enthalpy of dissolution	$\mathrm{Jmol}^{-1}$
$H_{\rm s}$	Henry solubility (all variants)	miscellaneous
$H_{\mathrm{s}}^{\ominus}$	Henry solubility at the reference temperature $T^{\ominus}$	miscellaneous
$H_{\rm s}^{bp}$	Henry solubility (defined as $b/p$ )	$\mathrm{mol}\mathrm{kg}^{-1};\mathrm{Pa}^{-1}$
$H_{\rm s}^{cc}$	Henry solubility (defined as $c/c$ )	1
$H_{\rm s}^{cp}$	Henry solubility (defined as $c/p$ )	$\mathrm{mol}\mathrm{m}^{-3}\mathrm{Pa}^{-1}$
$H_{\rm s,eff}$	effective Henry solubility	miscellaneous
$H_{\rm s}'$		miscellaneous
	$H \times K_{A} \xrightarrow{H_{s}} K_{A}$ (for strong acids)	
$H_{\rm v}$	Henry volatility (all variants)	miscellaneous
$H^{\ominus}_{\rm v}$	Henry volatility at the reference temperature $T^{\ominus}$	miscellaneous
$H_{\rm v}^{cc}$	Henry volatility (defined as $c/c$ )	1
$H_{\rm v}^{pc}$	Henry volatility (defined as $p/c$ )	${\rm Pa}{\rm m}^3{\rm mol}^{-1}$
$H_{\mathrm{v}}^{px}$	Henry volatility (defined as $p/x$ )	Pa
$K_{\mathrm{A}}$	acid constant	$ m molm^{-3}$
$K_{s}$		miscellaneous
	Sechenov parameter	
M	molar mass	$\mathrm{kgmol}^{-1}$
p	partial pressure $= c_g RT$	Pa
$p_{ m sat}$	saturation vapor pressure of water	Pa
<i>m</i>	saturation valor pressure of water	Pa
$p_{ m tot}$	total pressure (solute + water)	1 a
R	gas constant	$8.314\rm Jmol^{-1}K^{-1}$
T	temperature	Κ
$T^{\ominus}$	reference temperature	298.15 K
w	mass fraction in the aqueous phase	$\mathrm{kg}\mathrm{kg}^{-1}$ (dimensionless)
x	amount fraction (molar mixing ratio) in the aqueous phase	$mol mol^{-1}$ (dimensionless)
y	amount fraction (molar mixing ratio) in the gas phase	$mol mol^{-1}$ (dimensionless)

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\*A unit of "1" denotes a quantity of dimension 1, commonly called "dimensionless quantity".

where  $H_s^{\ominus} = \exp(A) \times \exp(B/T^{\ominus})$ . The enthalpy of dissolution  $\Delta_{sol}H$  is independent of temperature here:

$$\frac{-\Delta_{\rm sol}H}{R} = \frac{\mathrm{d}\ln H_{\rm s}}{\mathrm{d}(1/T)} = B \tag{6}$$

In this work, the values  $H_{\rm s}^{\ominus}$  and  ${\rm d}\ln H_{\rm s}/{\rm d}(1/T)$  are tabulated.

A simple equation based on the two parameters A and B is valid only for a limited temperature range, in which the enthalpy
of dissolution Δ<sub>sol</sub>H can be considered constant. To accommodate a larger temperature range, a third parameter C is often added:

$$\ln H_{\rm s} = A + \frac{B}{T} + C \times \ln T. \tag{7}$$

Here, the fit parameters A and B are different from those calculated for function (3). The enthalpy of dissolution  $\Delta_{sol}H$  changes linearly with temperature in the 3-parameter fit:

85 
$$\frac{-\Delta_{\rm sol}H}{R} = \frac{\mathrm{d}\ln H_{\rm s}}{\mathrm{d}(1/T)} = B - CT$$
(8)

To cover an even larger temperature range with an empirical formula, the dependence of  $\ln H_s$  on T can be expressed as the sum of several terms. For example, Wilhelm et al. (1977) used the formula:

$$\ln H_{\rm s} = A + B \times T^{-1} + C \times \ln T + D \times T. \tag{9}$$

The analytical derivative is simply the sum of the derivatives of the individual terms. Using the derivatives from Table 6, the 90 temperature dependence of this expression can be calculated as:

$$\frac{\mathrm{d\ln}H_{\mathrm{s}}}{\mathrm{d}(1/T)} = 0 + B - C \times T - D \times T^{2}.$$
(10)

When reporting Henry's law constants as such a function, it is important to present sufficient significant digits because  $H_s$  depends exponentially on the parameters.

Note that the temperature dependences for  $H_s^{cp}$  and  $H_s^{cc}$  are different since the conversion factor between them includes the 95 temperature:

$$\begin{aligned}
H_{s}^{cp} &= H_{s}^{cc}/(RT) \\
\Leftrightarrow \ln H_{s}^{cp} &= \ln H_{s}^{cc} + \ln(1/R) + \ln(1/T) \\
\Rightarrow \frac{\dim H_{s}^{cp}}{d(1/T)} &= \frac{\dim H_{s}^{cc}}{d(1/T)} + \frac{\dim(1/T)}{d(1/T)} \\
&= \frac{\dim H_{s}^{cc}}{d(1/T)} + T.
\end{aligned}$$
(11)

#### 100 2.5 Effective Henry's law solubility constants $H_{s,eff}$

The Henry's law constants mentioned so far describe the equilibrium between a chemical species in the gas phase and exactly the same species in the aqueous phase. This type is called the "intrinsic" Henry's law constant.

**Table 6.** Temperature-dependent terms and their analytical derivatives. Here, C,  $C_1$  and  $C_2$  are the empirical fit parameters defining  $\ln(H_s) \ln H_s$ . See Sect. 2.4 for details.

$\frac{\ln(H_s)}{\log H_s}$	$\frac{\mathrm{d} \ln H_{\mathrm{s}}}{\mathrm{d}(1/T)}$
C	0
C/T	C
CT	$-CT^2$
$CT^2$	$-2CT^3$
$C/T^2$	2C/T
$C/T^3$	$3C/T^2$
$C\ln(T)$	-CT
$C_1 \ln(C_2 T)$	$-C_1T$ (independent of $C_2$ )
$C\log_{10}(T)$	$-CT/\ln(10)$

Once transferredinto the aqueous phase, some species are involved in fast equilibria. In these cases, react in the aqueous phase. If these chemical reactions are fast and result in irreversible destruction, Henry's law cannot be applied. If, however,

105 the species enters a fast equilibrium in the aqueous-phase, it is possible to define an "effective" Henry's law constant  $H_{s,eff}$  and be defined, using a "total concentration"  $c_{tot}$ . Depending on the chemical class, there are different ways to define such a total concentration.

#### 2.5.1 $H_{s,eff}$ for aldehydes

Aldehydes can be hydrated, forming geminal diols. For example, methanal (HCHO) is almost completely hydrated in aqueous 110 solution:

 $HCHO + H_2O \rightleftharpoons H_2C(OH)_2 \tag{12}$ 

The total concentration of dissolved methanal is:

$$c_{\text{tot}} = c(\text{HCHO}) + c(\text{H}_2\text{C(OH)}_2)$$
(13)

The intrinsic Henry's law solubility constant of HCHO is:

115 
$$H_{\rm s} = \frac{c({\rm HCHO})}{p({\rm HCHO})}$$
(14)

In contrast, the effective Henry's law constant  $H_{s,eff}$  is defined as:

$$H_{\text{s,eff}} = \frac{c_{\text{tot}}}{p(\text{HCHO})} = \frac{c(\text{HCHO}) + c(\text{H}_2\text{C}(\text{OH})_2)}{p(\text{HCHO})}$$
(15)

#### 2.5.2 $H_{s,eff}$ for acids and bases

Acids and bases undergo ionic dissociation upon dissolution, e.g.:

$$120 \quad \mathrm{HCl} \rightleftharpoons \mathrm{H}^{+} + \mathrm{Cl}^{-} \tag{16}$$

Defining the total concentration  $c_{\rm tot}$  as

$$c_{\rm tot} = c({\rm HCl}) + c({\rm Cl}^-),\tag{17}$$

the effective Henry's law constant is:

$$H_{\text{s,eff}} = \frac{c_{\text{tot}}}{p(\text{HCl})} = \frac{c(\text{HCl}) + c(\text{Cl}^{-})}{p(\text{HCl})}$$
(18)

125 Considering the acidity constant

$$K_{\rm a} = \frac{c(\mathrm{H}^+) c(\mathrm{Cl}^-)}{c(\mathrm{HCl})},\tag{19}$$

the relation between the intrinsic and the effective Henry's law constant for HCl can be written as:

$$H_{\rm s,eff} = H_{\rm s} \times \left(1 + \frac{K_{\rm a}}{c({\rm H}^+)}\right) \tag{20}$$

Since the factor on the right-hand side contains  $c(H^+)$ , the conversion between the intrinsic and the effective Henry's law

130 constant is pH-dependent. Thus, effective Henry's law constants of acids and bases are not material constants but depend on solution pH. Proportionality between p(HCl) and  $c_{tot}$  is restricted to conditions under which the uptake of gaseous HCl does not affect the acidity of the solution. Thus, effective Henry's law constants of acids and bases are not material constants but depend on the solution pH (Sander et al., 2022).

In order to obtain a pH-independent constant, the product of the intrinsic Henry's law constant  $H_s^{cp}$  and the acidity constant 135  $K_a$  is often used for HCl and other strong acids:

$$H'_{\rm s} = H^{cp}_{\rm s} \times K_{\rm a} = \frac{c({\rm H}^+) \times c({\rm Cl}^-)}{p({\rm HCl})}$$
(21)

Although  $H'_s$  is usually also called a Henry's law constant, it should be noted that it is a different quantity and it has different units than  $H^{cp}_s$ .

#### 2.5.3 $H_{\rm s,eff}$ for halogens

140 In the aqueous phase, halogens are in equilibrium with their hypohalous acids, e.g.:

$$Cl_2 + H_2O \rightleftharpoons HOCl + H^+ + Cl^-.$$
<sup>(22)</sup>

The equilibrium constant is:

$$K = \frac{c(\text{HOCl})c(\text{H}^+)c(\text{Cl}^-)}{c(\text{Cl}_2)}$$
(23)

Since the sum of  $Cl_2$  and HOCl is not affected by this equilibrium, a "total chlorine concentration"  $c_{tot}$  can be defined as:

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$$c_{\text{tot}} = c(\text{Cl}_2) + c(\text{HOCl}),$$
 (24)

Using  $c_{tot}$ , it is formally possible to define an effective Henry's law constant as:

$$H_{\text{s,eff}} = \frac{c_{\text{tot}}}{p(\text{Cl}_2)} = \frac{c(\text{Cl}_2) + c(\text{HOCl})}{p(\text{Cl}_2)}$$
(25)

However, this definition is problematic because it doesn't work at infinite dilution. With decreasing Cl<sub>2</sub> concentration, the equilibrium in Eq. (22) will shift to the right (Le Chatelier's principle), i.e., c(HOCl) ≫ c(Cl<sub>2</sub>), and the effective Henry's law
solubility constant goes to infinity (see, e.g., Fig. 2 in Jones (1911) or Fig. A1 in Lin and Pehkonen (1998)). Therefore, the intrinsic Henry's law constant should be used for halogens, and the term "effective Henry's law constant" should be avoided here.

Instead of extrapolating to infinite dilution, the total chlorine solubility is sometimes reported at the fixed partial pressure of  $p(Cl_2) = 101325$  Pa. However, even in the vicinity of 101325 Pa, the total chlorine concentration  $c_{tot}$  is not proportional to 155  $p(Cl_2)$ .

In order to convert experimentally determined chlorine solubilities to the intrinsic constant  $H_s(Cl_2)$ , additional processes may have to be considered, e.g., aqueous-phase diffusion (Brian et al., 1962; Leaist, 1986) and the formation of chlorine hydrates (Adams and Edmonds, 1937; Young, 1983).

#### 2.6 Dependence of Henry's law constants on the composition of the solution

- Values of Henry's law constants for aqueous solutions depend on the composition of the solution, i.e., on its ionic strength and on dissolved organics. In general, the solubility of a gas decreases with increasing salinity ("salting out"). However, a "salting in" effect has also been observed, e.g., for the effective Henry's law constant of glyoxal (Kampf et al., 2013; Kurtén et al., 2015). The effect can be described with the Sechenov equation (Setschenow, 1889). Note that the scientific transliteration from Cyrillic is "Sechenov" but the original article was written in German and used the German transliteration "Setschenow". There
- 165 are many alternative ways to define the Sechenov equation, depending on how the aqueous-phase composition is described (based on concentration, molality, or molar amount fraction) and which variant of the Henry's law constant is used. Describing the solution in terms of molality is preferred because molality is invariant to temperature and to the addition of dry salt to the solution (see Sander (1999) for details). Thus, the Sechenov equation can be written as:

$$\log_{10}\left(\frac{H_{s0}^{bp}}{H_{s}^{bp}}\right) = K_{s} \times b(\text{salt})$$
(26)

170 where  $H_{s0}^{bp}$  = Henry's law constant in pure water,  $H_s^{bp}$  = Henry's law constant in the salt solution,  $K_s$  = molality-based Sechenov constant parameter for a given salt, and b(salt) = molality of the salt. For mixed electrolyte solutions with more than one salt, an extension of the Sechenov equation developed by Schumpe (1993) and Weisenberger and Schumpe (1996) can be used. Sechenov parameters are not suitable for systems in which a species reacts irreversibly with the salt (e.g., N<sub>2</sub>O<sub>5</sub> + Cl<sup>-</sup>). Since the atmosphere contains very dilute cloud droplets as well as highly concentrated aerosols, adequate values of Henry's law constants should be used. Unfortunately, Sechenov parameters are unknown for many species.

#### 3 Values of Henry's law constants

#### **3.1** The data compilation

The compilation of Henry's law constants is presented in the appendix, and it will also be is also available online at https://www.henrys-law.org. It contains Henry's law constants for inorganic and organic species of potential importance in environmental chemistry. Most data were measured at ambient conditions (around 298 K and 1 atm). Data at high temperatures are excluded or (if possible) extrapolated to  $T^{\ominus} = 298.15$  K. The data refer to aqueous solutions; octanol and other solvents are not included considered. The constants refer to pure water as solvent unless noted otherwise (e.g., sea water).

All Henry's law constants have been converted to a uniform format:  $H_s^{cp}$  with the unit mol/(m<sup>3</sup> Pa). In cases where the conversion involves the temperature-dependent density of water, the parameterization by Bettin and Spieweck (1990) was used

185 to calculate  $\rho_{H_2O}$  at the temperature *T*. The temperature-dependent vapor pressure of water  $p_{sat}$  was calculated using the parameterization by Buck (1981).

Inorganic substances are sorted according to the elements they contain. The order chosen is: O, H, N, F, Cl, Br, I, S, rare gases, others. Compounds with several of these elements are put into the last of the applicable sections. For example, nitryl chloride which contains O, N and Cl, is listed in the Cl section. Carbon-containing compounds (including CO and CO<sub>2</sub>) are sorted somewhat arbitrarily by increasing chain length and complexity. Hetero atoms (O, N, F, Cl, Br, I, S, P, etc.) are sorted in the same order as for inorganic compounds. The table contains the following groups of species:

The first column of the table shows the systematic name, the chemical formula, trivial names (if any), the CAS registry number (in square brackets), and the InChIKey.

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The column labeled " $H_s^{cp}$ " contains Henry's law solubility constants at the reference temperature  $T^{\ominus} = 298.15$  K. Values are rounded to two significant digits and given in the unit mol/(m<sup>3</sup> Pa).

The column labeled " $d\ln H_s/d(1/T)$ " contains the temperature dependence of the Henry solubility as defined in Eq. (5), rounded to two significant digits and given in the unit K. If the term  $\Delta_{sol}H$  is temperature-dependent, the value of  $d\ln H_s/d(1/T)$  is calculated at  $T^{\ominus} = 298.15$  K. If a 3-parameter fit according to Eq. (7) allows the parameterization over a larger temperature range, it is presented in the notes.

- For each table entry the column labeled "type" denotes how the Henry's law constant was obtained in the given reference. Literature reviews are usually most reliable, followed by original publications of experimental determinations of  $H_s$ . Other data has to be treated more carefully. The types listed here are roughly ordered by decreasing reliability: <u>Note, however, that</u> recent measurements which are newer than the latest review article should always be considered.
  - "L" The cited paper is a *literature* review.

- "M" Original publication of a *measured* value. 205
  - "V" Vapor pressure of the pure substance divided by aqueous solubility (sometimes called "VP/AS").
  - "**R**" The cited paper presents a *recalculation* of previously published material (e.g. extrapolation to a different temperature or concentration range).
  - "T" Thermodynamical calculation ( $\Delta_{sol}G = -RT \ln H$ , see Sander (1999) for details).
- "X" The original paper was not available for this study. The data listed here was were found in a secondary source. 210
  - "C" The paper is a *citation* of a reference which I could not obtain (personal communication, Ph.D. theses, grey literature).
  - "O" The value was calculated with using a "quantitative structure property relationship" (QSPR) or a similar theoretical method.
  - "E" The value is an *estimate*. Estimates are listed only if no reliable data are available.
- "?" The cited paper doesn't clearly state how the value was obtained. 215
  - "W" The value is probably wrong, as explained in the notewrong. It is not listed in the table, in order to avoid spreading of erroneous data. More information can be found in the notes.

In some cases there might be good agreement between different authors. However, if the original work they refer to is not known one has to be careful when evaluating the reliability. It is possible that they were recalculating data from the same source. The similarity in that case would not be due to independent investigations. 220

The table entries in the pdf of this document are hyperlinked to endnotes with additional information. In order to avoid spreading of erroneous data, some of these notes identify errors in the original publications. Symbols and acronyms used here refer to those in the original publications.

The CAS numbers in the tables are hyperlinked to the NIST Chemistry WebBook.

#### 225 3.2 Further sources of information

#### 3.2.1 Review articles

Several reviews about Henry's law have been published, starting with Markham and Kobe (1941), up to more recent publications such as Wilhelm et al. (1977), Mackay and Shiu (1981), Staudinger and Roberts (1996), Staudinger and Roberts (2001), Fogg and Sangster (2003), and Burkholder et al. (2019). Practical guidance on the use of Henry's law has been published by Smith and Harvey (2007).

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Experimental methods to obtain Henry's law constants as well as indirect (theoretical) methods have been described and compared by several authors. Only a brief summary of some articles is given here. For details, the reader is referred to the original publications:

- Battino and Clever (1966): Miscellaneous methods, partially of historical interest
- 235 - Betterton (1992): Head-space method, bubble column method, thermodynamic cycles, calculation from vapor pressure and solubility, linear correlations
  - Turner et al. (1996): Static methods, mechanical recirculation methods, separate measurement of solubility and pure species vapor pressure, ebulliometry, perturbation chromatography
- Staudinger and Roberts (1996): Batch air stripping, concurrent flow technique, Equilibrium Partitioning in Closed Systems (EPICS), calculation via Quantitative Property Property Relationships (OPPR), Quantitative Structure Property 240 Relationships (QSPR), UNIversal quasichemical Functional group Activity Coefficients (UNIFAC)
  - Brennan et al. (1998): Comparison of predictive methods
  - Sander (1999): OPPR, OSPR, thermodynamic calculations
  - Fogg and Sangster (2003): Miscellaneous methods
- 245 - Dupeux et al. (2022): QSPR

#### 3.2.2 Internet

On the internet, several pages provide Henry's law constants, e.g.:

- The PubChem database: https://pubchem.ncbi.nlm.nih.gov
- 250 - The NIST Chemistry WebBook: https://webbook.nist.gov/chemistry
  - The ChemSpider database: https://www.chemspider.com
- The Generator for Explicit Chemistry and Kinetics of Organics in the Atmosphere (GECKO-A) provides Henry's law 255 constants on the basis of experimental data and structure-activity relationships: http://geckoa.lisa.u-pec.fr/generateur form.php
  - The Pesticide Properties Database (PPD): https://www.ars.usda.gov/Services/docs.htm?docid=14199
  - HENRYWIN, a program to calculate Henry's law constants:
  - https://www.epa.gov/tsca-screening-tools/epi-suitetm-estimation-program-interface

- Vapor-liquid equilibrium data (mostly at elevated temperatures) from the "Dortmund Data Bank": http://www.ddbst.com/en/EED/VLE/VLEindex.php
- EPI Suite estimates from the Arctic Monitoring and Assessment Programme (AMAP) database: https://chemicals.amap.no/about

#### 265 3.2.3 Vapor-liquid equilibrium data

Henry's law constants can be obtained from vapor-liquid equilibrium (VLE) data. For example, consider a binary mixture that consists of a solute dissolved in water. The total pressure  $P_{p_{tot}}$  over the solution is the sum of the partial pressures of the components. The partial pressure of the solute can be defined via Henry's law, and the partial pressure of the water can be defined via Raoult's law:

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$$\underline{Pp_{tot}} = p_{solute} + p_{water}$$
$$= xH_v^{px} + (1-x)p_{sat}$$
$$= x(H_v^{px} - p_{sat}) + p_{sat}$$
(27)

where  $p_{sat}$  is the saturation vapor pressure of water. If VLE data with the total pressure at several small solute fractions x are available, the derivative  $\frac{dP/dx}{dp_{tot}/dx}$  (i.e., the slope of a plot  $\frac{P}{p_{tot}}$  vs x) can be used to obtain the Henry's law constant:

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$$\frac{\mathrm{d}P}{\mathrm{d}x}\frac{\mathrm{d}p_{\mathrm{tot}}}{\mathrm{d}x} = H_{\mathrm{v}}^{px} - p_{\mathrm{sat}} \Rightarrow H_{\mathrm{v}}^{px} = \frac{\mathrm{d}P}{\mathrm{d}x}\frac{\mathrm{d}p_{\mathrm{tot}}}{\mathrm{d}x} + p_{\mathrm{sat}}$$
(28)

#### 4 The electronic supplement

The Supplement contains several files with additional information about the compiled Henry's law constants. It includes a README file with a detailed description. Here, only a short summary is given:

- The files henry\_\*.f90 contain the Fortran 90 code that was used to convert the values from the original publications to a uniform format : the uniform format  $H_s^{cp}$  with the unit mol/(m<sup>3</sup> Pa). The code and the comments in the code can be used to double-check that the conversion was done correctly.
  - If the original publications contain measurements at different temperatures, the code often contains all individual data points, not just the regression line that was used to calculate the temperature dependence. In addition, the supplement contains data files with the temperature-dependent values of  $H_s^{cp}$  in output/Tdep\_data/\*.dat and plots of the data points as well as the regression lines according to Eqs. (5) and (7) in output/gnuplot/Tdep.pdf.
  - If the Henry's law constants are needed in electronic form, it is cumbersome to extract them from the pdf of this article. Therefore, the supplement contains the files output/\*.f90 with declarations of the Henry's law constants  $(H_s^{cp}, H_s^{xp}, H_s^{bp}, H_s^{cc}, H_v^{pc}, H_v^{px}, \text{ and } H_v^{cc})$  in Fortran 90 syntax.

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- For some references, the util/ directory contains python scripts that preprocess input and perform other calculations related to the original data.

#### 5 Summary and outlook

An updated and extended version of a compilation of Henry's law constants has been presented. The collection, which will also be is also available at https://www.henrys-law.org, will be continously maintained, updated and extended in the future. If necessary, errata will also be posted on the web page. In addition to providing a source of information, I hope that this work will help to identify gaps in our current knowledge and stimulate research projects. In particular, it seems that even for some well-known chemicals like isoprene. HCl, Br<sub>2</sub>, and or BrCl, there is a large uncertainty in the value of the Henry's law constants. I always welcome information emails informing me about new measurements of Henry's law constants to be included in the table.

Supplement. The supplement related to this article is available online at: https://doi.org/10.5194/jn-0-1-2023-supplement.

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Appendix A: Appendix with data tables

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